

Petroleum Geology · Engineering · Hydrogeologu · Regulatory Permittina

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June 15, 2015

NSR Program Manager / attn: O&G Production Facilities Permit Application Department of Environmental Quality Air Quality Division

Herschler Building, 2-E 122 West 25th Street Chevenne, WY 82002

RE: Peak Powder River Resources, LLC

Chapter 6 Section 2 Air Quality Permit Application

Van Buggenum 1-2H

Dear Program Manager:

Enclosed are one hard copy and one electronic copy of the Air Quality Permit Application for the facility named above, prepared on behalf of our client Peak Powder River Resources, LLC who is requesting a waiver for this facility since there are no emission sources requiring control to meet the Presumptive BACT requirements described in the Chapter 6 Section 2 Oil and Gas Production Facilities Permitting Guidance (C6 S2 Guidance). This is a new single well production facility located in Campbell County, within the "Statewide Area" that is defined in the C6 S2 Guidance.

The First Date of Production per the definition in the C6 S2 Guidance was March 24, 2015, making this application due June 24, 2015. The application has been prepared in accordance with the September 2013 O&G Permitting Guidance.

Please contact me if additional information or clarification is needed.

Sincerely, ynthia Madison Cynthia Madison **Project Engineer**

Attachment

CD

CC: Modeler



STATE OF WYOMING

Department of Environmental Quality/Air Quality Division C6 S2 Air Quality Permit Application



Peak Powder River Resources, LLC

Van Buggenum 1-2H

API 49-005-61581 Latitude: 43.737071 Longitude: -105.837423 SE SW Section 35, Township 44N, Range 75W Campbell County, WY



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Process Description

The Van Buggenum 1-2H is a new horizontal well producing from the Shannon Formation. The well is located in Campbell County within the area specified as "Statewide" in the Chapter 6, Section 2 Oil and Gas Production Facilities Permitting Guidance (C6 S2 Guidance). The well is designated as Wildcat by the Wyoming Oil and Gas Conservation Commission

The well initially came on line on March 18, 2015 but did not produce consistently until March 24, 2015 therefore; for Air Quality permitting purposes the First Date of Production (FDOP) was March 24, 2015.

The well is produced by an electric pumping unit. Well fluids are routed into a high pressure 2-phase separator. Gas off the separator is metered and routed into a high pressure sales line. The fluids move on to a heater treater with a 0.5 million Btu per hour (MMBTU/HR) burner. The gas stream off the treater is metered and routed into the low pressure sales line. Oil and water are routed to four 400-barrel (BBL) oil tanks and one 400-BBL water tank and are eventually hauled away by truck for sales and disposal. Vapors from the oil tanks are collected and routed to a smokeless combustor for destruction of the volatile organic compound (VOC) and hazardous air pollutant (HAP) components. Because uncontrolled tank emissions are below the Presumptive BACT control level, the combustor may be removed. There is a dual head flare for flaring the produced gas during emergency or upset conditions.

An electric pump circulates oil from the storage tanks back through the production equipment if further treatment is necessary.

There are no pneumatic pumps or process controllers used at this location.

Presumptive BACT

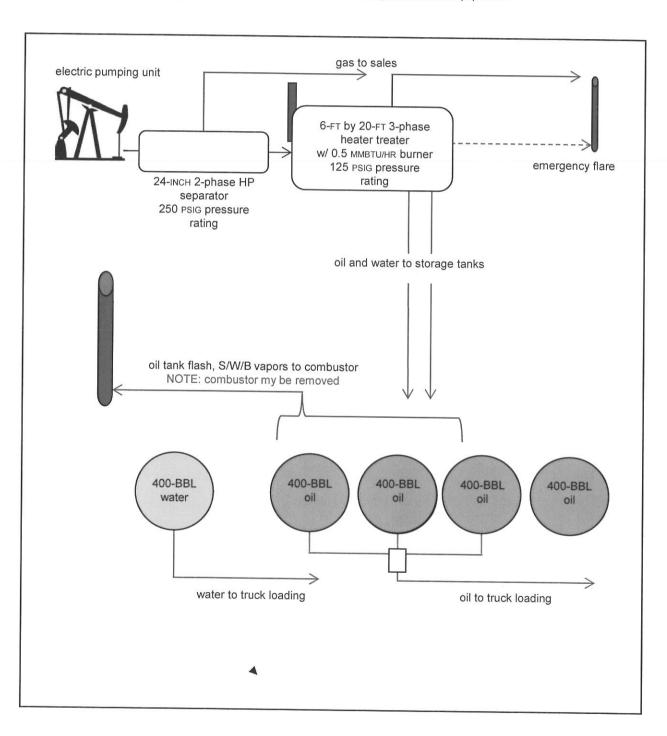
The sources at this facility that are affected by the Presumptive BACT requirements in the C6 S2 Guidance are the oil tanks. Within 60-days of the FDOP, flashing emissions containing greater than or equal to 10 tons per year (TPY) of VOC shall be controlled by at least 98%. Presumptive BACT requirements also include monitoring and recordkeeping which will demonstrate continuous and effective emission control.

Vapors from the tanks are collected and routed to a smokeless combustor which was in place upon startup of the facility. The combustor is designed to achieve greater than 99% destruction efficiency and is designed to be compliant with EPA NSPS 40 CFR Part 60, Subpart OOOO (see Pages 14-16). Operation of the combustor is continually recorded and monitored using a SCADA type system. Since the projected rate of VOC emissions from the tanks is less than 10 TPY, BACT requirements are met with no control and the combustor may be removed.

There are no pneumatic controllers or pumps and there are no other sources at this facility emitting ≥8 TPY of VOC or ≥5 TPY of hazardous air pollutants (HAP) that would require a BACT analysis to be filed with this application. All Presumptive BACT requirements specified in the C6 S2 Guidance for "Statewide Area" production facilities have been met.

Process Diagram Van Buggenum 1-2H

Diagram does not represent actual scale or placement of equipment.



Emission Calculations

Flash & S/W/B

The API E&P TANK V2 model was used to estimate uncontrolled tank emissions. The model was run using the projected oil production rate and average hydrocarbon composition of Shannon oil from Peaks nearby wells (see Page 11). The text file generated by the model run is shown below.

| *** | ******** | ******************** |
|---|---|---|
| * | Project Setup Information | * |
| **** | ******** | ******************* |
| | ect File: | |
| | sheet Selection: | Oil Tank with Separator |
| | ulation Method: | RVP Distillation |
| | rol Efficiency: | 0% |
| | wn Separator Stream: | Low Pressure Oil |
| Ente | ring Air Composition: | No |
| Filed | Name: | Peak Powder River Resources, LLC |
| Well | Name: | Van Buggenum 1-2H |
| Well | ID: | |
| Pern | nit Number: | Air Quality Permit Application |
| Date | : | 2015.06.11 |
| | | |
| **** | ******* | ************************************** |
| | Data Input | * |
| | | ******************* |
| | | |
| | rator Pressure: | 30.00 [psig] |
| | rator Temperature: | 130.00 [F] |
| | ient Pressure: | 12.00 [psia] |
| Amb | ient Temperature: | 50.00 [F] |
| | CC. | |
| C10+ | | 0.80365 |
| C10+ | SG: MW: | 0.80365 235.884 |
| C10+ C10+ | | |
| C10+ C10+ | MW: | |
| C10+ C10+ Lov No. 1 | MW: v Pressure Oil | 235.884 |
| C10+ C10+ Lov No. 1 2 | MW: w Pressure Oil Component H2S O2 | 235.884 mol % |
| C10+ C10+ Lov No. 1 2 | MW: V Pressure Oil Component H2S O2 CO2 | 235.884 |
| C10+ C10+ Lov No. 1 2 3 4 | MW: V Pressure Oil Component H2S O2 CO2 N2 | 235.884 mol % 0.0000 0.0000 0.0560 0.0020 |
| C10+ C10+ Lov No. 1 2 3 4 5 | MW: V Pressure Oil Component H2S O2 CO2 N2 C1 | 235.884 mol % 0.0000 0.0000 0.0560 0.0020 0.8000 |
| C10+ C10+ Lov No. 1 2 3 4 5 6 | MW: V Pressure Oil Component H2S O2 CO2 N2 C1 C2 | 235.884 mol % 0.0000 0.0000 0.0560 0.0020 0.8000 0.3720 |
| C10+ C10+ Lov No. 1 2 3 4 5 6 7 | MW: V Pressure Oil Component H2S O2 CO2 N2 C1 C2 C3 | 235.884 mol % 0.0000 0.0000 0.0560 0.0020 0.8000 0.3720 1.3250 |
| C10+ C10+ Lov No. 1 2 3 4 5 6 7 8 | MW: V Pressure Oil Component H2S O2 CO2 N2 C1 C2 C3 i-C4 | mol % 0.0000 0.0000 0.0560 0.0020 0.8000 0.3720 1.3250 0.6030 |
| C10+ C10+ Lov No. 1 2 3 4 5 6 7 8 9 | MW: v Pressure Oil Component H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 | 235.884 mol % 0.0000 0.0000 0.0560 0.0020 0.8000 0.3720 1.3250 0.6030 2.0260 |
| C10+ C10+ Lov No. 1 2 3 4 5 6 7 8 9 10 | MW: v Pressure Oil Component H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 | 235.884 mol % 0.0000 0.0000 0.0560 0.0020 0.8000 0.3720 1.3250 0.6030 2.0260 1.0590 |
| C10+ C10+ Lov No. 1 2 3 4 5 6 7 8 9 10 | MW: N Pressure Oil Component H2S O2 C02 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 | 235.884 mol % 0.0000 0.0000 0.0560 0.0020 0.8000 0.3720 1.3250 0.6030 2.0260 1.0590 1.4350 |
| C10+ C10+ Lov No. 1 2 3 4 5 6 7 8 9 10 11 12 | MW: N Pressure Oil Component H2S O2 C02 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 | 235.884 mol % 0.0000 0.0000 0.0050 0.0020 0.8000 0.3720 1.3250 0.6030 2.0260 1.0590 1.4350 1.1860 |
| C10+ C10+ Lov No. 1 2 3 4 5 6 7 8 9 10 11 12 13 | MW: N Pressure Oil Component H2S O2 C02 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 | 235.884 mol % 0.0000 0.0000 0.0560 0.0020 0.8000 0.3720 1.3250 0.6030 2.0260 1.0590 1.4350 1.1860 5.2860 |
| C10+ C10+ Lov No. 1 2 3 4 5 6 7 8 9 10 11 12 | MW: N Pressure Oil Component H2S O2 C02 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 | 235.884 mol % 0.0000 0.0000 0.0560 0.0020 0.8000 0.3720 1.3250 0.6030 2.0260 1.0590 1.4350 1.1860 5.2860 13.6970 |
| C10+ C10+ Lov No. 1 2 3 4 5 6 7 8 9 10 11 12 13 14 | MW: w Pressure Oil Component H2S O2 C02 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 | 235.884 mol % 0.0000 0.0000 0.0560 0.0020 0.8000 0.3720 1.3250 0.6030 2.0260 1.0590 1.4350 1.1860 5.2860 |
| C10+ C10+ C10+ Lov No. 1 2 3 4 5 6 6 7 8 9 10 11 12 13 14 15 | MW: w Pressure Oil Component H2S O2 C02 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 | 235.884 mol % 0.0000 0.0000 0.0560 0.0020 0.8000 0.3720 1.3250 0.6030 2.0260 1.0590 1.4350 1.1860 5.2860 13.6970 8.7900 |
| C10+ C10+ C10+ Lov No. 1 2 3 4 5 6 6 7 8 9 10 11 12 13 14 15 16 | MW: w Pressure Oil Component H2S O2 C02 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ | 235.884 mol % 0.0000 0.0000 0.0560 0.0020 0.8000 0.3720 1.3250 0.6030 2.0260 1.0590 1.4350 1.1860 5.2860 13.6970 8.7900 59.1820 |
| C10+ C10+ C10+ Lov No. 1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 | MW: w Pressure Oil Component H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 c6 C7 C8 C9 C10+ Benzene | mol % 0.0000 0.0000 0.0560 0.0020 0.8000 0.3720 1.3250 0.6030 2.0260 1.0590 1.4350 1.1860 5.2860 13.6970 8.7900 59.1820 0.1340 |
| C10+ C10+ C10+ Lov No. 1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 | MW: W Pressure Oil Component H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 C6 C7 C8 C9 C10+ Benzene Toluene | mol % 0.0000 0.0000 0.0560 0.0020 0.8000 0.3720 1.3250 0.6030 2.0260 1.0590 1.4350 1.1860 5.2860 13.6970 8.7900 59.1820 0.1340 0.5860 |
| C10+ C10+ C10+ Lov No. 1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 | MW: v Pressure Oil Component H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene | mol % 0.0000 0.0000 0.00560 0.0020 0.8000 0.3720 1.3250 0.6030 2.0260 1.0590 1.4350 1.1860 5.2860 13.6970 8.7900 59.1820 0.1340 0.5860 0.1370 |

| Sales Oil | | | | | | | | |
|----------------------|-----------|-----------|----------|-----------|----------|-----------|---------|-----------------|
| Production Rate: | | 214 [bbl/ | | | | | | |
| Days of Annual Oper | ation: | 365 [day: | | | | | | |
| API Gravity: | ation. | 35.0 | s/ year] | | | | | |
| Reid Vapor Pressure | | 7.80 [psi | al | | | | | |
| rela vapor i ressare | | 7.00 [psi | *1 | | | | | |
| ****** | ******* | ****** | ******* | ****** | ****** | ****** | ****** | ***** |
| * Calculation Resu | | | | * | | | | |
| ****** | ****** | ****** | ******* | ****** | ****** | ****** | ****** | ***** |
| Emission Summary | / | | | | | | | |
| Item | Uncontro | lled Unco | ntrolled | | | | | |
| | [ton/yr] | | [lb/hr] | | | | | |
| Total HAPs | 0.090 | | 0.021 | | | | | |
| Total HC | 12.024 | | 2.745 | | | | | |
| VOCs, C2+ | 7.069 | | 1.614 | | | | | |
| VOCs, C3+ | 5.562 | | 1.270 | | | | | |
| Uncontrolled Recove | ny Info | | | | | | | |
| Vapor | | x1E-3 [MS | CED] | | | | | |
| HC Vapor | | x1E-3 [MS | | | | | | |
| GOR | 4.62 [SCF | | CFDJ | | | | | |
| GOIN | 4.02 [30] | / DDI] | | | | | | |
| Emission Composit | tion | | | | | | | |
| No Component | Uncontro | | Uncontro | | | | | |
| | [ton/yr] | | [lb/hr] | | | | | |
| 1 H2S | 0.000 | | 0.000 | | | | | |
| 2 02 | 0.000 | | 0.000 | | | | | |
| 3 CO2 | 0.519 | | 0.118 | | | | | |
| 4 N2 | 0.030 | | 0.007 | | | | | |
| 5 C1 | 4.954 | | 1.131 | | | | | |
| 6 C2 | 1.508 | | 0.344 | | | | | |
| 7 C3 | 2.557 | | 0.584 | | | | | |
| 8 i-C4 | 0.585 | | 0.134 | | | | | |
| 9 n-C4 | 1.370 | | 0.313 | | | | | |
| 10 i-C5 | 0.316 | | 0.072 | | | | | |
| 11 n-C5 | 0.312 | | 0.071 | | | | | |
| 12 C6 | 0.079 | | 0.018 | | | | | |
| 13 C7 | 0.125 | | 0.029 | | | | | |
| 14 C8 | 0.108 | | 0.025 | | | | | |
| 15 C9 | 0.024 | | 0.005 | | | | | |
| 16 C10+ | 0.000 | | 0.000 | | | | | |
| 17 Benzene | 0.006 | | 0.001 | | | | | |
| 18 Toluene | 0.008 | | 0.002 | | | | | |
| 19 E-Benzene | 0.001 | | 0.000 | | | | | |
| 20 Xylenes | 0.009 | | 0.002 | | | | | |
| 21 n-C6 | 0.055 | | 0.013 | | | | | |
| 22 224Trimethylp | 0.007 | | 0.002 | | | | | |
| Total | 12.573 | | 2.871 | | | | | |
| Stream Data | | | | | | | | |
| No. Component | | MW | LP Oil | Flash Oil | Sale Oil | Flash Gas | W&S Gas | Total Emissions |
| | | | mol % | mol % | mol % | mol % | mol % | mol % |
| 1 H2S | | 34.80 | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0.0000 |
| 2 02 | | 32.00 | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0.0000 |
| 3 CO2 | | 44.01 | 0.0560 | 0.0374 | 0.0374 | 2.4741 | 0.0000 | 2.4741 |
| 4 N2 | | 28.01 | 0.0020 | 0.0003 | 0.0003 | 0.2212 | 0.0000 | 0.2212 |
| 5 C1 | | 16.04 | 0.8000 | 0.3069 | 0.3069 | 64.8138 | 0.0000 | 64.8138 |
| 6 C2 | | 30.07 | 0.3720 | 0.2938 | 0.2938 | 10.5226 | 0.0000 | 10.5226 |
| 7 C3 | | 44.10 | 1.3250 | 1.2415 | 1.2415 | 12.1693 | 0.0000 | 12.1693 |
| 8 i-C4 | | 58.12 | 0.6030 | 0.5914 | 0.5914 | 2.1107 | 0.0000 | 2.1107 |
| 9 n-C4 | | 58.12 | 2.0260 | 2.0035 | 2.0035 | 4.9459 | 0.0000 | 4.9459 |
| 10 i-C5 | | 72.15 | 1.0590 | 1.0601 | 1.0601 | 0.9196 | 0.0000 | 0.9196 |
| 11 n-C5 | | 72.15 | 1.4350 | 1.4390 | 1.4390 | 0.9079 | 0.0000 | 0.9079 |
| 12 C6 | | 86.16 | 1.1860 | 1.1936 | 1.1936 | 0.1982 | 0.0000 | 0.1982 |
| 13 C7 | | 100.20 | 5.2860 | 5.3246 | 5.3246 | 0.2715 | 0.0000 | 0.2715 |

100.20 5.2860 5.3246 5.3246 0.2715 0.0000 0.2715

| 14 C8 | 114.23 | 13.6970 | 13.8008 | 13.8008 | 0.2041 | 0.0000 | 0.2041 |
|---------------------------|--------|---------|---------|---------|---------|--------|---------|
| 15 C9 | 128.28 | 8.7900 | 8.8573 | 8.8573 | 0.0418 | 0.0000 | 0.0418 |
| 16 C10+ | 235.88 | 59.1820 | 59.6372 | 59.6372 | 0.0000 | 0.0000 | 0.0000 |
| 17 Benzene | 78.11 | 0.1340 | 0.1349 | 0.1349 | 0.0170 | 0.0000 | 0.0170 |
| 18 Toluene | 92.13 | 0.5860 | 0.5904 | 0.5904 | 0.0191 | 0.0000 | 0.0191 |
| 19 E-Benzene | 106.17 | 0.1370 | 0.1380 | 0.1380 | 0.0014 | 0.0000 | 0.0014 |
| 20 Xylenes | 106.17 | 1.9760 | 1.9911 | 1.9911 | 0.0168 | 0.0000 | 0.0168 |
| 21 n-C6 | 86.18 | 1.0400 | 1.0470 | 1.0470 | 0.1328 | 0.0000 | 0.1328 |
| 22 224Trimethylpentane | 114.24 | 0.3090 | 0.3113 | 0.3113 | 0.0123 | 0.0000 | 0.0123 |
| | | | | | | | |
| MW | | 180.12 | 181.31 | 181.31 | 26.39 | 0.00 | 26.39 |
| Stream Mole Ratio | | 1.0000 | 0.9924 | 0.9924 | 0.0076 | 0.0000 | 0.0076 |
| Heating Value [BTU/SCF] | | | | | 1499.50 | 0.00 | 1499.50 |
| Gas Gravity [Gas/Air] | | | | | 0.91 | 0.00 | 0.91 |
| Bubble Pt. @ 100 F [psia] | 33.31 | 17.13 | 17.13 | | | | |
| RVP @ 100F [psia] | 7.97 | 6.08 | 6.08 | | | | |
| Spec. Gravity @ 100 F | 0.696 | 0.696 | 0.696 | | | | |
| | | | | | | | |

Total Uncontrolled Tank Emissions

5.56 TPY VOC and 0.09 TPY HAP

Treater Burner

Fuel gas for the 0.5 MMBTU/HR heater treater burner comes from the well. Emissions were calculated using AP-42 emission factors (100 LB $NO_X/MMCF$ and 84 LB CO/MMCF) and the average heat content of Shannon produced gas from Peaks nearby wells (see Page 12). For the purposes of this application, it is assumed the burner operates 8760 hours annually.

 NO_X (TPY) = 0.5 MMBTU/HR (100 LB NO_X /MMCF)(1322 BTU/1020 BTU)(1 SCF/1020 BTU)(8760 HR/YR) (TON/2000 LB) = 0.28 TPY NO_X

CO (TPY) = 0.5 MMBTU/HR (84 LB CO/MMCF)(1322 BTU/1020 BTU)(1 SCF/1020 BTU)(8760 HR/YR) (TON/2000 LB) = 0.23 TPY CO

Fugitives

The typical component count for a Peak single well production facility, the fugitive emission factors provided in the C6 S2 Guidance and the corresponding weight percentages of VOC and HAP in the produced gas (see Page 12) were used to estimate fugitive emissions.

| Emission Factors | | | | | | | | | | |
|-------------------------|---------|---------------|--------|-------|--------------|--------|--------|---------------|--------|--|
| Equipment Type | Gas | | | Ligh | t Oil | | Wat | er/Light Oil | | |
| | LB Th | HC/DAY/compon | ent | LB Th | HC/DAY/compo | nent | | HC/DAY/compon | ent | |
| Connector | 0.01 | 10 | | 0.01 | | | 0.00 | | CIIL | |
| Flange | 0.02 | 10 | | 0.00 | 58 | | 0.0002 | | | |
| Open line | 0.11 | 00 | | 0.07 | 40 | | 0.0130 | | | |
| Other | 0.47 | 00 | | 0.40 | 00 | | 0.7400 | | | |
| Pump | 0.13 | 00 | | | 0.6900 | | | 0.0013 | | |
| Valve | 0.24 | 00 | | 0.13 | | | 0.00 | | | |
| Component Coun | t and S | ervice Type | | | | | 0.00. | <i>5</i> 2 | | |
| | No. | LB THC/DAY | TPY | No. | LB THC/DAY | TPY | No. | LB THC/DAY | TPY | |
| Connector | 30 | 0.3300 | 0.0602 | 60 | 0.6600 | 0.1204 | 30 | 0.1740 | 0.0317 | |
| Flange | 10 | 0.2100 | 0.0383 | 20 | 0.1160 | 0.0212 | 10 | 0.0020 | 0.0004 | |
| Open line | 0 | 0.0000 | 0.0000 | 0 | 0.0000 | 0.0000 | 0 | 0.0000 | | |
| Other | 4 | 1.8800 | 0.3431 | 8 | 3.2000 | 1.1680 | 4 | 2.9600 | 0.0000 | |
| Pump | 0 | 0.0000 | 0.0000 | 0 | 0 | 0 | 1 | 0.0013 | 0.5402 | |
| Valve | 20 | 4.8000 | 0.8760 | 40 | 5.2000 | 0.9490 | 20 | 0.1040 | 0.0002 | |
| SUBTOTALS | | | 1.32 | | 5.2000 | 2.26 | 20 | 0.1040 | 0.0190 | |

Total THC = 4.17 TPY

4.17 TPY (33.551/100) = 1.40 TPY VOC

 $4.47 \text{ TPY } (2.206/100) = \underline{0.10 \text{ TPY HAP}}$

Truck Loading

Truck loading emissions are estimated using the method described in the C6 S2 Guidance, the projected daily oil production rate and the oil tank vapor properties estimated by the E&P TANK Model (see Page 13).

| projected BOPD> BBL/YR | 214 * 365 = 7 | 8,110 BBL/YR |
|--|---------------|--------------|
| saturation factor (submerged loading, normal svc.) | 0.6 | S |
| true vapor pressure of oil @ T = 50°F | 2.3 | Р |
| molecular weight of tank vapors (LB/LB-MOL) | 26.4141 | M |
| temperature (°R) | 510 | Т |
| VOC content of tank vapors | 66.89 WT% | |
| HAP content of tank vapors | 0.68 WT% | |

LL = 12.46 * S * P * M/T = 12.46 * 0.6 * 2.3 * 26.4141/510 = 0.89 LB/1000 GAL 0.89 LB/1000 GAL loaded (42 GAL/BBL) (78,110 BBL/YR) (TON/2000 LB) = 1.46 TPY total losses

1.46 TPY (66.89/100) = **0.98 TPY VOC**

 $1.46 \text{ TPY } (0.68/100) = \underline{0.01 \text{ TPY HAP}}$

Emission Summary

Total Estimated Uncontrolled Emissions (Tons Per Year)

| EMISSION SOURCE | VOCs | total HAPs | NO _x | со | SO ₂ | H₂S |
|-----------------|------|------------|-----------------|------|-----------------|-----|
| oil tanks | 5.56 | 0.09 | | | | |
| burner | | | 0.28 | 0.23 | | |
| fugitives | 0.14 | 0.10 | 0.20 | 0.20 | | |
| truck loading | 0.98 | 0.01 | | | | |
| | | | | | | |
| TOTAL | 6.68 | 0.10 | 0.28 | 0.23 | | |

Total Estimated Controlled Emissions (Tons Per Year)

| EMISSION SOURCE | VOCs | total HAPs | NO _x | со | SO ₂ | H₂S |
|-----------------|------|------------|-----------------|----|-----------------|-----|
| | | | | | | |
| | | | | | | |
| | | | | | | |
| | | | | | | |
| | | | | | | |

Hazardous Air Pollutants (TPY)

| SOURCE | Benzene | Toluene | Ethyl-Benzene | Xylenes | Othe |
|--------|---------|---------|---------------|---------|------|
| | | | | | |

Production Record

| Date | PODD | | |
|------------------------|------------|--------------------------------------|----------|
| | BOPD | | BWPD |
| 4/27/2015 | | | 174 |
| 4/26/2015 | | | 132 |
| 4/25/2015 | - | | 119 |
| 4/24/2015 | |) | 100 |
| 4/23/2015 | 299 | | 96 |
| 4/22/2015 | 391 | | 177 |
| 4/21/2015 4/20/2015 | 293 | | 197 |
| 4/20/2015 | 444 | | 146 |
| 4/18/2015 | 530 | | 107 |
| 4/17/2015 | 203 | | 150 |
| 4/17/2015 | 374 | | 161 |
| 4/15/2015 | 312 | | 116 |
| 4/14/2015 | 496 | | 161 |
| 4/13/2015 | 370 | | 117 |
| 4/12/2015 | 398 351 | | 131 |
| 4/11/2015 | 446 | | 155 |
| 4/10/2015 | 415 | | 150 |
| 4/9/2015 | 289 | Initial 20 day avers | 164 |
| 4/8/2015 | 305 | Initial 30-day average = 356 BOPD | 40 |
| 4/7/2015 | 473 | - 220 ROAD | 55 |
| 4/6/2015 | 369 | | 101 |
| 4/5/2015 | 266 | | 40 |
| 4/4/2015 | 231 | 356 * 0.6 | 120 |
| 4/3/2015 | 202 | = 214 BOPD projected | 49 39 |
| 4/2/2015 | 314 | 227 boi b projected | 95 |
| 4/1/2015 | 395 | | 148 |
| 3/31/2015 | 267 | | 108 |
| 3/30/2015 | 409 | | 200 |
| 3/29/2015 | 332 | | 173 |
| 3/28/2015 | 379 | | 218 |
| 3/27/2015 | 121 | | 525 |
| 3/26/2015 | 314 | | 72 |
| 3/25/2015 | 322 | | 42 |
| 3/24/2015 | 761 | | 364 |
| 3/23/2015 | 75 | | 555 |
| 3/22/2015 | 0 | | 0 |
| 3/21/2015 | 0 | | 0 |
| 3/20/2015 | 151 | | 1081 |
| 3/19/2015 | 213 | | 1165 |
| 3/18/2015 | 267 | | 0 |

SHANNON OIL

| | IBERLIN 1-4H | PUMPKIN BUTT | ES PUMPKIN BUTTI | ES | | ATWOOD LAUR | 1- | |
|------------------------|--------------|--------------|------------------------|-------------|--------------|-------------|------------|------------------|
| Components | - | 1-3H | 1-27H | ROUSH 1-21H | SPOMER 1-18H | | LUKE 1-34H | A M 1 . 0 |
| II.d. a ICI | Mole % | Mole % | Mole % | Mole % | Mole % | Mole % | Mole % | — Average Mole % |
| Hydrogen Sulfide | 0.000 | 0.000 | 0.000 | 0.000 | 0.000 | 0.000 | 0.000 | 0.000 |
| Oxygen | 0.000 | 0.000 | 0.000 | 0.000 | 0.000 | 0.000 | 0.000 | 0.000 |
| Carbon Dioxide | 0.026 | 0.026 | 0.032 | 0.042 | 0.012 | 0.054 | 0.198 | 0.056 |
| Nitrogen | 0.003 | 0.001 | 0.001 | 0.001 | 0.001 | 0.001 | 0.006 | 0.002 |
| Methane | 0.313 | 0.285 | 0.507 | 1.180 | 0.189 | 1.139 | 1.984 | 0.800 |
| Ethane | 0.308 | 0.176 | 0.184 | 0.752 | 0.265 | 0.672 | 0.246 | 0.372 |
| Propane | 1.197 | 0.802 | 0.470 | 2.650 | 1.174 | 2.183 | 0.797 | |
| iso-Butane | 0.692 | 0.597 | 0.378 | 0.742 | 0.398 | 0.598 | 0.816 | 1.325 |
| n-Butane | 2.803 | 2.071 | 0.782 | 2.416 | 1.590 | 2.633 | 1.884 | 0.603 |
| iso-Pentane | 1.352 | 1.135 | 0.687 | 1.020 | 0.916 | 1.052 | 1.248 | 2.026 |
| n-Pentane | 1.989 | 1.418 | 0.756 | 1.593 | 1.303 | 1.567 | 1.419 | 1.059 |
| Hexanes | 1.206 | 0.938 | 0.842 | 1.586 | 1.097 | 1.358 | 1.419 | 1.435 |
| Heptanes | 6.437 | 3.945 | 2.773 | 7.003 | 5.438 | 5.920 | | 1.186 |
| Octanes | 13.152 | 11.631 | 11.158 | 17.410 | 16.021 | 14.586 | 5.487 | 5.286 |
| Nonanes | 8.715 | 8.487 | 7.304 | 9.695 | 9.240 | 9.714 | 11.924 | 13.697 |
| Decanes+ | 57.191 | 64.618 | 71.857 | 47.615 | 57.838 | | 8.377 | 8.790 |
| Benzene | 0.192 | 0.081 | 0.033 | 0.315 | 0.133 | 54.469 | 60.687 | 59.182 |
| Toluene | 0.670 | 0.472 | 0.189 | 0.923 | 0.586 | 0.121 | 0.062 | 0.134 |
| Ethylbenzene | 0.083 | 0.169 | 0.052 | 0.259 | 0.071 | 0.574 | 0.690 | 0.586 |
| (ylenes | 1.869 | 1.852 | 1.231 | 3.278 | 2.104 | 0.095 | 0.231 | 0.137 |
| n-Hexane | 1.442 | 1.007 | 0.636 | 1.117 | | 2.025 | 1.471 | 1.976 |
| 2,2,4-Trimethylpentane | 0.360 | 0.289 | 0.128 | 0.403 | 1.296 | 0.868 | 0.917 | 1.040 |
| Totals | 100.000 | 100.000 | 100.000 | | 0.328 | 0.371 | 0.281 | 0.309 |
| | 100.000 | 100.000 | 100.000 | 100.000 | 100.000 | 100.000 | 100.000 | 100.000 |
| emp F | 128 | 146 | 140 | 120 | 150 | 100 | | |
| ressure PSIG | 38 | 34 | 25 | 10 | | 108 | 112 | 129 |
| Date | 2/14/2013 | 5/8/2013 | 6/24/2013 | | 28 | 5 | 94 | 33 |
| | 2/14/2015 | 3/0/2013 | 6/24/2013 | 9/27/2013 | 4/4/2013 | 9/11/2013 | 3/20/2014 | |
| PI GRAVITY (sales oil) | 38.4 | 34.6 | 31.6 | 36.8 | 38.2 | 37.5 | 20.2 | |
| G OF C10+ | 0.79217 | 0.82177 | 0.82894 | 0.78459 | 0.80734 | | 28.2 | 35.043 |
| VERAGE MW Oil | 185.409 | 194.194 | 207.783 | | N. 1 E - 10 | 0.79603 | 0.79470 | 0.80365 |
| VERAGE MW of C10+ | 248.466904 | 243.839 | Long to the State To a | 152.645 | 181.031 | 165.617 | 186.783 | 181.923 |
| ALES RVP | 7.6 | | 247.485 | 210.736 | 236.265 | 220.695 | 243.698 | 235.884 |
| ALLO IVVE | 7.0 | 5.6 | 4.1 | 9.1 | 9.7 | 7.2 | 4.6 | 7.8 |

The gas gathering line pressures, which dictate the operating pressures of the treaters, variy widely in this production area. This is why pressures of the oil samples vary more than is normally seen for samples taken from a group of similar wells producing from one formation. Because the mol percent values for the components of the above samples are very similar, regardless of sample pressure, the calculated 'average analysis' is appropriate for use in modeling tank emissions from Peak's Shannon wells.

Note: The two lowest values for RVP of sales oil are excluded from the average.

SHANNON GAS

| | Components Carbon Dioxide Hydrogen Sulfide Nitrogen Methane Ethane Propane iso-Butane n-Butane iso-Pentane | 1-20H Mole % 1.302 0 1.038 | Mole % | Mole % | 1-3H Mole % | 1-27H Mole % | Mole % | AVERAGE Mol% | |
|--|--|--|--------|--------|--|--|--------|-----------------|---|
| Components Mole ⅓ Mole ⅓ Mole ⅓ Mole ⅓ Mole ⅓ Mole ⅓ Lása Componental Lása 1,988 1,393 1,453 Componental 1,998 1,393 1,453 Componental 1,998 1,393 1,451 Lasa Lydrogen 0 0,000 | Carbon Dioxide | 1.302 0 1.038 | 1.383 | | the second secon | The second secon | | Mol% | |
| Carbon Dioxide | Carbon Dioxide | 1.302 0 1.038 | 1.383 | | the second secon | The second secon | | | |
| Nytrogen 1.038 | Hydrogen Sulfide Nitrogen Methane Ethane Propane iso-Butane n-Butane iso-Pentane | 0 1.038 | | 0.984 | 1 657 | | | | |
| Nitrogen | Nitrogen Methane Ethane Propane soo-Butane n-Butane iso-Pentane | 1.038 | 0.000 | | | | 1.393 | 1.453 | |
| Methane | Methane Ethane Propane iso-Butane n-Butane iso-Pentane | | | | | | | 0.000 | |
| Ethane | Ethane Propane iso-Butane n-Butane iso-Pentane | | | | | | | | |
| Propage | Propane iso-Butane n-Butane iso-Pentane | | | | | | 72.604 | 74.544 | |
| So-Butane | iso-Butane n-Butane iso-Pentane | | | | | | 9.381 | 8.121 | |
| n-Butane | n-Butane iso-Pentane | | | | 8.475 | 6.529 | 9.208 | 8.480 | |
| So-Pentane | iso-Pentane | | | | | 1.98 | 1.207 | 1.292 | |
| n-Pentane | | | | | 2.819 | 2.205 | 2.861 | 2.727 | |
| Cyclopentane 0.026 0.022 0.025 0.023 0.034 0.007 0.023 n-Hexane 0.169 0.186 0.162 0.154 0.261 0.203 0.189 Cyclohexane 0.041 0.036 0.040 0.034 0.07 0.046 0.045 Other Hexanes 0.142 0.209 0.238 0.197 0.346 0.228 0.227 Heptanes 0.104 0.102 0.149 0.175 0.211 0.183 0.154 Methylcyclohexane 0.039 0.032 0.047 0.052 0.045 0.052 0.045 2,2,4-Trimethylpentane 0.013 0.018 0.018 0.023 0.027 0.030 0.022 2,2,4-Trimethylpentane 0.001 0.008 0.009 0.004 0.003 0.002 0.007 0.003 0.002 Tolune 0.019 0.008 0.023 0.008 0.009 0.003 0.002 0.001 0.001 0.001 0.001 0.00 | | | | 0.675 | 0.685 | 0.895 | 0.683 | 0.702 | |
| N-Hexane | | | 0.693 | 0.703 | 0.618 | 0.702 | 0.695 | 0.670 | |
| Cyclohexane 0.041 0.036 0.040 0.034 0.07 0.046 0.045 Other Hexanes 0.142 0.209 0.238 0.197 0.346 0.228 0.227 Heptanes 0.104 0.102 0.149 0.175 0.211 0.183 0.154 Methylcyclohexane 0.039 0.032 0.047 0.052 0.045 0.052 0.045 2,2,4-Trimethylpentane 0.013 0.018 0.018 0.023 0.027 0.030 0.022 Benzene 0.008 0.006 0.009 0.004 0.003 0.009 0.007 Toluene 0.019 0.008 0.023 0.008 0.009 0.023 0.015 Ethylbenzene 0.001 0.000 0.001 0.000 0.001 0.001 0.003 0.001 Sylenes 0.011 0.004 0.010 0.006 0.011 0.001 1.00 100 100 100 100 100 100 100 | | 0.026 | 0.022 | 0.025 | 0.023 | 0.034 | 0.007 | 0.023 | |
| Other Hexanes 0.142 0.209 0.238 0.197 0.346 0.228 0.227 Heptanes 0.104 0.102 0.149 0.175 0.211 0.183 0.154 Methylcyclohexane 0.033 0.047 0.052 0.045 2,2,4-Trimethylpentane 0.013 0.018 0.018 0.023 0.027 0.030 0.022 Benzene 0.008 0.006 0.009 0.004 0.003 0.009 0.001 Toluene 0.019 0.008 0.023 0.001 0.001 0.003 0.002 Kylenes 0.001 0.003 0.001 0.006 0.011 0.011 0.001 C8+ Heavies 0.034 0.039 0.051 0.036 0.056 0.026 0.040 Totals 100 100 100 100 100 100 100 100 100 100 100 100 100 100 100 100 100 100 100 | | 0.169 | 0.186 | 0.162 | 0.154 | 0.261 | 0.203 | 0.189 | |
| Heptanes | | 0.041 | 0.036 | 0.040 | 0.034 | 0.07 | 0.046 | 0.045 | |
| Methylcyclohexane | Other Hexanes | 0.142 | 0.209 | 0.238 | 0.197 | 0.346 | 0.228 | 0.227 | |
| Methylcyclohexane | Heptanes | 0.104 | 0.102 | 0.149 | 0.175 | 0.211 | 0.183 | | |
| 2,2,4-Trimethylpentane 0.013 0.018 0.018 0.023 0.027 0.030 0.022 Benzene 0.008 0.006 0.009 0.004 0.003 0.009 0.023 Toluene | Methylcyclohexane | 0.039 | 0.032 | 0.047 | 0.052 | 0.045 | 0.052 | | |
| Decider Components Weight Weigh | 2,2,4-Trimethylpentane. | . 0.013 | 0.018 | 0.018 | 0.023 | 0.027 | | | |
| Toluene | Benzene | 0.008 | 0.006 | 0.009 | | | | | |
| Ethylbenzene | | | | | | | | | |
| Xylenes | | | | | | | | | |
| Carbon Dioxide | | | | | | | | | |
| Totals | | | | | | | | | |
| Sample temperature (°F) 50 128 150 146 140 50 sample pressure (PSIG) 5 38 28 34 25 5 molecular weight 23.283 23.747 22.635 22.927 22.800 23.578 23.162 BTU wet basis (BTU/SCF) 1335 1362 1305 1302 1280 1347 1322 sample date 8/30/2013 2/14/2013 3/27/2013 5/7/2013 6/20/2013 9/27/2013 Components Weight % | | | | | | | | | _ |
| sample pressure (PSIG) 5 38 28 34 25 5 molecular weight 23.283 23.747 22.635 22.927 22.800 23.578 23.162 BTU wet basis (BTU/SCF) 1335 1362 1305 1302 1280 1347 1322 sample date 8/30/2013 2/14/2013 3/27/2013 5/7/2013 6/20/2013 9/27/2013 Components Weight % 13.20< | | | 100 | 100 | 100 | 100 | 100 | 100 | |
| molecular weight 23.283 23.747 22.635 22.927 22.800 23.578 23.162 BTU wet basis (BTU/SCF) 1335 1362 1305 1302 1280 1347 1322 sample date 8/30/2013 2/14/2013 3/27/2013 5/7/2013 6/20/2013 9/27/2013 Components Weight % | | | | | | | | | |

MOL% to WEIGHT% Conversion

Shannon Tank Vapors

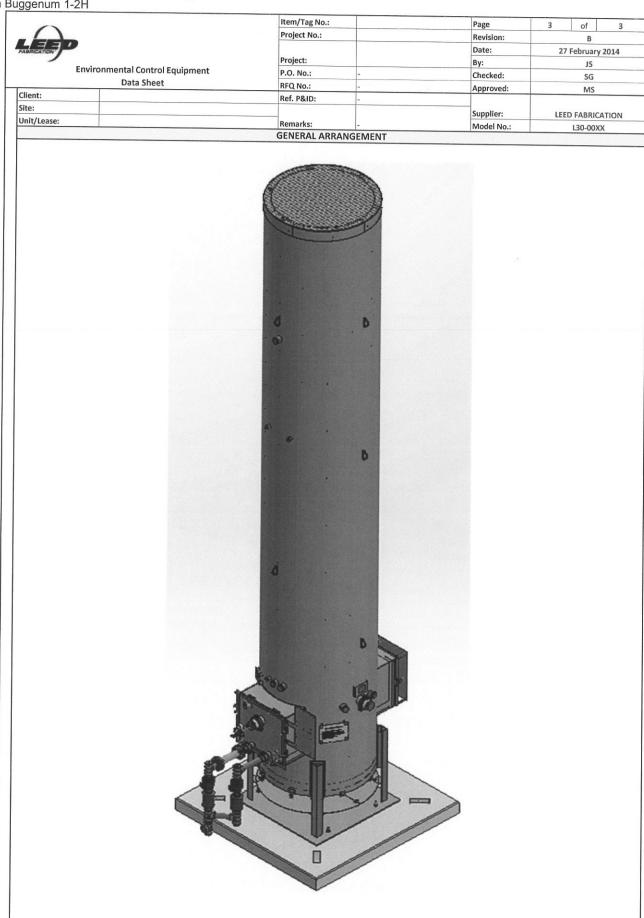
from E&P TANK output

Composition of "Total Emissions" from E&P TANK

| COMPONENT | mol % | | M.W. | (mol % X MW)/100 | WT% of i | | |
|------------------------|-----------------------------|----------------------|------------|------------------|----------|--|--|
| H2S | 0 | 1 | 34.08 | 0 | 0 | | |
| 02 | 0 | | 32.00 | 0 | 0.0000 | | |
| CO2 | 2.4741 | | 44.01 | 1.0889 | 0.0412 | | |
| N2 | 0.2212 | | 28.02 | 0.0620 | 0.0023 | | |
| Methane C1 | 64.8138 | | 16.04 | 10.3961 | 0.3936 | | |
| Ethane C2 | 10.5226 | | 30.07 | 3.1641 | 0.1198 | | |
| Propane C3 | 12.1693 | | 44.09 | 5.3654 | 0.2031 | | |
| i-Butane i-C4 | 2.1107 | | 58.12 | 1.2267 | 0.0464 | | |
| n-Butane n-C4 | 4.9459 | | 58.12 | 2.8746 | 0.1088 | | |
| i-Pentane iC5 | 0.9196 | | 72.15 | 0.6635 | 0.0251 | | |
| n-Pentane nC5 | 0.9079 | | 72.15 | 0.6550 | 0.0248 | | |
| n-Hexane n-C6 | 0.1328 | | 86.17 | 0.1144 | 0.0043 | | |
| Cyclohexane | 0 | composition of tank | 84.16 | 0.0000 | 0.0000 | | |
| other Hexanes | 0.1982 | vapors from E&P TANK | 85.00 | 0.1685 | 0.0064 | | |
| Heptanes | 0.2715 | MODEL | 100.20 | 0.2720 | 0.0103 | | |
| Methylcyclohexane | 0 | | 98.18 | 0.0000 | 0.0000 | | |
| 2,2,4 Trimethylpentane | 0.0123 | | 114.22 | 0.0140 | 0.0005 | | |
| Benzene | 0.017 | | 78.11 | 0.0133 | 0.0005 | | |
| Toluene | 0.0191 | | 92.14 | 0.0176 | 0.0007 | | |
| Ethylbenzene | 0.0014 | | 106.17 | 0.0015 | 0.0001 | | |
| Xylenes | 0.0168 | | 106.17 | 0.0178 | 0.0007 | | |
| C8 | 0.2041 | | 120.00 | 0.2449 | 0.1957 | | |
| C9 | 0.0418 | | 128.26 | 0.0536 | 0.0414 | | |
| C ₁₀ + | 0 | | 142.29 | 0.0000 | 0.0000 | | |
| hydrogen | 0 | | 1.01 | 0.0000 | 0.0000 | | |
| Helium | 0 | | 4.00 | 0.0000 | 0.0000 | | |
| water | 0 _ | | 18.02 | 0.0000 | 0.0000 | | |
| | 100 | | | | 1.2258 | | |
| | M | OLECULAR WEIGHT (I | b/lb-mol)= | 26.4141 | | | |
| | ТО | TAL VOCs WEIGHT PE | RCENT = | 0.6689 | | | |
| | TOTAL HAPs WEIGHT PERCENT = | | | | | | |

| _ | - POW 75 R | | | - | | | | | | | |
|----|-------------------------|--|-------------------|------------|----------------------|------------|----------------|--------------|------------------|----------|--------------|
| | | Item/Tag No. | | |).: | | Page | | 1 | of | 3 |
| | Project No.: | | | | | Revis | sion: | | В | | |
| ١, | LEED | | | | | | Date | : | 27 F | ebruary | 2014 |
| ' | FABRICATION . | | | Project: | | | Ву: | | | JS | |
| | Enviro | onmental Control Equipment | | P.O. No.: | | | Chec | kod: | | SG | |
| | | Data Sheet | | RFQ No.: | | | | oved: | | 0.00000 | |
| Н | Client: | Ref. P&ID: | | | | | Аррг | ovea: | | MS | |
| | Site: | | | Rei. PaiD: | | | | | | | |
| | | | | | | | Supp | | | FABRICA | |
| | Unit/Lease: | | | Remarks: | - - | | Mod | el No.: | | L30-00XX | (|
| ١. | Deeles Cada | | | GE | NERAL | | | | | | |
| | Design Code: | | | | | NDE: | | ı | EED Fabricat | ion Stan | dards |
| 2 | Service: | | | | | Custom | er Specs: | | Yes | | |
| 3 | Description: | | | | | | | | ✓ No | | |
| | | | | PROC | ESS DATA | | | | | | |
| | Gas Composition: | | | | Process Conditions: | | | | | | |
| | das composition. | | | mol % | Variable | | Value | Unit | ts | NEW WAR | |
| 4 | Methane | | | | Flow Rate | | | Msc | | | |
| 5 | Ethane | | | | Pressure | | | psig | | | |
| 6 | Propane | | | | Temperatur | 0 | | °F | | | |
| 7 | I-Butane | | | | | | | F | | | |
| 8 | | | | | Molecular We | | | | | | |
| 9 | n-Butane | | | | Process/Waste S | | ✓ Gas | | Liquid | | |
| | I-Pentane | | | | Detailed Process De | | | | | | |
| 10 | | | | | 1. Turndown 10:1. | | | nal operatir | ng rate indica | ted abov | /e. |
| 11 | | | | | 2. DRE: 98 % opera | | | | | | |
| 12 | | | | | 3. Burner Pressure | prop: Mi | n. 0.10 oz/in2 | | | | |
| 13 | N2 | | | | | | | | | | |
| 14 | Helium | | | | 1 | | | | | | |
| 15 | H ₂ O | | | | 1 | | | | | | |
| 16 | C7 | | | | 1 | | | | | | |
| 17 | C8 | | | | 1 | | | | | | |
| 18 | | | | | - | | | | | | |
| 19 | | | | | - | | | | | | |
| 20 | | | | | - | | | | | | |
| | | | | | - | | | | | | |
| 21 | | TOTAL | | | | | | | | | |
| | Other Components: | | | PPMV | Available Utilities: | | | | | | |
| 22 | H2S | | | | Fuel / Pilot G | as | ı | Min. 30psig | Natural Gas | /Propan | e 40-50 SCFI |
| 23 | Benzene | | | | Instrument A | ir | 1 | NA | | | |
| 24 | Toluene | | | | Power | | 1 | 120 V / 60 H | lz or Solar Po | wer | |
| 25 | E-Benzene | | | | Steam | | - | NA | | | |
| 26 | Xylene | | | | Purge Gas | | | | | | |
| | | | | DESIG | GN DATA | | | | | 951955 | |
| 27 | Ambient Temperatures | : | | | Noise Performance | Requirer | nonte: | T | Under | DE ADA | |
| 28 | | Low, °F | -21 | 0 | Structural Design Co | | nents. | _ | Onder | OJ UDA | |
| 29 | | High, °F | 12 | | | Jue. | | | 4000 | | |
| 30 | | Pressure/Temperature | 12 | | Wind Design Code: | | | | ASCE | | |
| | | | - | | | | | | | | |
| | Max. Relative Humidity | 7, 70 | 90 | J | | | e/Speed | | 100 mph | | |
| | Elevation (ASL), ft | | | nt a | L | Categor | У | | | | |
| | Area Classification: | | Class I | | Seismic Design Cod | | | | | | |
| 34 | Electrical Design Code: | and the second s | NE | | | Location | n | | | | |
| | | | | EQUIPMENT | SPECIFICATION | | | | | | |
| | Туре: | | inclosed | | Equipment Design: | | | | | | |
| 36 | | Above Ground | | | (| ompone | nt | Ma | aterial / Size / | Rating | / Other |
| 37 | | ✓ Stack ✓ M | Iultiple Stack | | Burner | | | | | | |
| 38 | | Portable / Trailer | | | Burner Tix | / Assist | Gas Burner | | | | |
| 39 | | | | | | urner Bo | | | | | |
| 40 | Smokeless By: | Steam A | ssist Air | | Pilot | | | | | | |
| 41 | | | taging | | 1 | Pilot Tip | <u> </u> | | | - | |
| 42 | | | | | — | ilot Line | | | | | |
| 43 | Stack: | Self Supporting | | | Firebox / Stack | not Line | -1 | | | | |
| 44 | Flare Burner: | | mokeless | Cas Assist | Literox / Stack | ct " | | | | | |
| 45 | Pilot: | ✓ Intermittent | Continuous | Gas Assist | | Shell | | - | | | |
| 46 | | Local | Remote | | | Piping | | + | | | |
| 47 | Pilot Air Inspirator: | | | unla) | | Nozzles | | | | | |
| | Pilot Flame Control: | ∐ No ✓ | Yes (Thermocol | upie) | | Flanges | | | | | |
| 48 | | | | | | Insulatio | | | | | |
| 49 | Pilot Ignition: | ☐ Flamefront Generator ✓ | Inspirating Ignit | | Ins | sulation F | Pins | | | | |
| 50 | | ☐ Electronic ✓ | Automatic | Manual | | Refractor | γ | | | | |
| 51 | | With Pilot Flame Control | | | Refra | actory An | ichors | | | | |
| 52 | | With Auto Pilot Re-Ignition | | | Ladde | rs and Pla | atforms | | | | |
| 53 | | - Control Control Harrison - Con | | | | | nnections | | | | |
| 54 | Pilot Ignition Backup: | Manual Specify: i.e P | iezo-Electric | | | Sight Glas | | | | | |
| 55 | | Battery Pack | | | | Other | | | | | |

| FABRICATION P | | Item/Tag No.: Project No.: | i | Page | 2 | of | |
|-----------------------------------|--|-------------------------------|---|-----------------------|----------|------------|------|
| PARKICATION" | | Project No.: | | Revision: | | В | |
| | ICATION" | | | Date: | 2 | 7 February | 2014 |
| Enviro | nmental Control Equipment | Project: P.O. No.: | _ | By: | | JS | |
| | Data Sheet | RFQ No.: | - | Checked: Approved: | | SG | |
| Client: | | Ref. P&ID: | - | Approved. | | MS | |
| Site: | | | | Supplier: | LEI | ED FABRIC | ΔΤΙΩ |
| Unit/Lease: | | Remarks: | - | Model No.: | | L30-00X | |
| Flame Detection: | ☐ Thermocouple ✓ Ioniz | | SPECIFICATION | | | | |
| riame Detection: | ☐ UV Scanner ✓ Ioniz | ration Rod | Auxiliary Equipment | | | | |
| General Configuration: | UV Scallie | | Valves | | | | |
| y the second | | } | Blowers | | | | |
| | | } | Dampers | | | | |
| | | ŀ | Inlet KO / Liquid Flame / Detonation | | | | |
| | | Ī | Instrumentation & Controls | Arrestor | | | |
| | | 1 | Solenoids / Shut-Of | f Valves | | | |
| | | 9 | Flow Meters | | | | |
| | | | Calorimeter | | | | |
| | | | Pressure Switches/Tra | insmitters | | | |
| | | L | Thermocouple | es | | | |
| | | - | Temperature Switches/1 | Fransmitters | | | |
| | | - | BMS | | | | |
| | 8 | - | CEMS | | | | |
| | Pro In | - | Other | | | | |
| | | F | | | | | |
| | 0 | | | | | | |
| | | | | | | | |
| | | FABRICATION A | ND INSPECTION | | | | |
| pecial requirements | Skid Mounted Concrete | Pad | | Equipment Info | | | |
| | Other | | Component | | Weight / | Dimension | ns |
| nspection | ✓ Vendor Standard | В | Burner | | | | |
| | Other. Specify: | | Burner Assemb | ly | | | |
| Naterial Certification | ✓ Vendor Standard | S | tack | | | | |
| | ☐ MTR | | Stack Assemble | У | | | |
| | Certificate of Compliance | | Pilot Tip Pilot Line(s) | | | | |
| | Other (Specify): | | Stack Assembly | , | | | |
| NDE | ✓ Vendor Standard | A | uxiliary Equipment | 4 | | | |
| | | | | | | | |
| | Radiography. Specify: | | Blowers | 1 2 | | | |
| | Ultrasonic. Specify: | | Inlet KO / Liquid S | Seal | | | |
| | Ultrasonic. Specify: Liquid Penetrant. | | | | | | |
| | Ultrasonic. Specify: Liquid Penetrant. Magnetic Particles. | | Inlet KO / Liquid S Flame / Detonation A Skid | | | | |
| | Ultrasonic. Specify: Liquid Penetrant. Magnetic Particles. PMI. Specify: | In | Inlet KO / Liquid S Flame / Detonation A | | | | |
| urface Preparation | Ultrasonic. Specify: Liquid Penetrant. Magnetic Particles. PMI. Specify: Other. Specify: | ln | Inlet KO / Liquid S Flame / Detonation A Skid | | | | |
| urface Preparation | Ultrasonic. Specify: Liquid Penetrant. Magnetic Particles. PMI. Specify: Other. Specify: Vendor Standard | ln | Inlet KO / Liquid S Flame / Detonation A Skid Istrumentation & Controls | | | | |
| urface Preparation aint System | Ultrasonic. Specify: Liquid Penetrant. Magnetic Particles. PMI. Specify: Other. Specify: | ln | Inlet KO / Liquid S Flame / Detonation A Skid Istrumentation & Controls BMS | | | | |
| | Ultrasonic. Specify: Liquid Penetrant. Magnetic Particles. PMI. Specify: Other. Specify: Vendor Standard Other. Specify: | ln | Inlet KO / Liquid S Flame / Detonation A Skid Istrumentation & Controls BMS | | | | |
| aint System | Ultrasonic. Specify: Liquid Penetrant. Magnetic Particles. PMI. Specify: Other. Specify: Vendor Standard Other. Specify: Vendor Standard | In | Inlet KO / Liquid S Flame / Detonation A Skid Istrumentation & Controls BMS | | | | |
| | Ultrasonic. Specify: Liquid Penetrant. Magnetic Particles. PMI. Specify: Other. Specify: Vendor Standard Other. Specify: Vendor Standard Other. Specify: Other. Specify: | In | Inlet KO / Liquid S Flame / Detonation A Skid Istrumentation & Controls BMS | | | | |
| aint System | Ultrasonic. Specify: Liquid Penetrant. Magnetic Particles. PMI. Specify: Other. Specify: Vendor Standard Other. Specify: Vendor Standard Other. Specify: Vendor Standard Other. Specify: Vendor Standard | In | Inlet KO / Liquid S Flame / Detonation A Skid Istrumentation & Controls BMS | | | | |



| П | Buggenum 1-2H | | | | | | | | | |
|----------|---------------------------|-----------------------------|---------------|-------------|-----------|---|----------------|----------|-------------|-------------------------------|
| | | | | Item/Tag N | 0.: | | | Page | | 1 of 3 |
| | | | | Project No. | : | | | Revisio | n: | В |
| | LEED | EED | | | | | | Date: | | |
| П | FABRICATION | | | Project: | | | | _ | - | 27 February 2014 |
| | Enviro | mental Control Equipment | | | | | | Ву: | | JS |
| 1 | | Data Sheet | | P.O. No.: | | - | | Checke | d: | SG |
| \vdash | Client | Data Silect | | RFQ No.: | | - | | Approv | ed: | MS |
| | Client: | | | Ref. P&ID: | | - | | | | |
| | Site: | | | | | | | Supplie | r: | LEED FABRICATION |
| 1 | Unit/Lease: | | | Remarks: | | ~ | | Model I | | |
| ı | | | | | ENERAL | | | woderi | VO.: | Dual Head Flare |
| 1 | Design Code: | | | | LIVELIAL | | | | | |
| 2 | Service: | | | | | NDE | | | LEI | ED Fabrication Standards |
| 3 | | | | | - | Cust | omer Specs: | | [| Yes |
| ľ | Description. | | Dual Hea | | | | | | [| ✓ No |
| | | | | PROC | CESS DAT | ΓΑ | | | | |
| | Gas Composition: | | | 10/ | Process | Conditions: | | | | |
| | | | | mol % | | Variable | Valu | 0 | Units | |
| 4 | Methane | | | | | Flow Rate | | | | |
| 5 | Ethane | | | | + | | 2.75 / | | mmSCFD | High Press. / mSCFD Low Press |
| 6 | | | | | | Pressure | 100 / | 16 | psig High | Press. / oz/in2 Low Press. |
| 7 | | | | | | Temperature | | | °F | |
| | | | | | Mo | olecular Weight | | | | |
| 8 | | | | | Proce | ess/Waste Stream | Gas | | | Liquid |
| 9 | I-Pentane | | | | | Process Descript | | nter | | |
| 10 | n-Pentane | | | | 1. Turne | lown 10:1 Based | on an owner to | no | | rate indicated above |
| 11 | n-Hexane | | | | 2. Gae n | nixture heating va | on an expected | normal | operating | rate indicated above |
| 12 | | | | | | | | o pe 150 | O B LO\2CE | #8 - |
| | | | | | | I gas composition ISPS 40 CFR Part (| | | | |
| 13 | | | | | 5. 98% E | | oo compliant | | | |
| 14 | | | | | 3. 98% L | JKE | | | | |
| 15 | H ₂ O | | | | 7 | | | | | |
| 16 | C7 | | | | 1 | | | | | |
| 17 | C8 | | | | - | | | | | |
| 18 | | | | | 4 | | | | | |
| | | | | | 1 | | | | | |
| 19 | | | | | | | | | | |
| 20 | C11+ | | | | | | | | | |
| 21 | | TOTAL | | | 1 | | | | | |
| | Other Components: | | | PPMV | Available | e Utilities: | | | | |
| 22 | H2S | | | | | | | | | |
| 23 | Benzene | | | | | el / Pilot Gas | Natural Gas: | 40 SCFH | / Propane | e 30 SCFH @ 5-7 psig |
| 24 | | | | | In | strument Air | | NA | | |
| | Toluene | | | | | Power | | 120 | V / 60 Hz c | or Solar Power |
| 25 | E-Benzene | | | | | Steam | | NA | | |
| 26 | Xylene | | | | | Purge Gas | | NA | | |
| | | | | DESIG | SN DATA | | | 1110 | | |
| 27 | Ambient Temperatures: | | | D.510 | | | | | | |
| 28 | | Low, °F | | -20 | | rformance Requi | rements: | | | |
| 29 | | High, °F | | | | al Design Code: | | | | |
| | D. J. C. IIII | | | 120 | Wind De | sign Code: | | | | ASCE |
| | Design Conditions: | Pressure/Temperature | | | | | | | | |
| | Max. Relative Humidity, % | 6 | | 90 | | Press | ure/Speed | | | 100 mph |
| 32 | Elevation (ASL), ft | | | | | Categ | | - | | |
| 33 | Area Classification: | | Cla | ass I Div 2 | Seismir F | Design Code: | 1 | | | |
| 34 | Electrical Design Code: | | 211 | NEC | - STATE L | | 1 | | | |
| | <u> </u> | | | | CDECIE | Locat | ion | | | |
| 35 l | Type: | ✓ Elevated ☐ E | nclosed | EQUIPMENT | | | | | | |
| - 1 | .,,,, | | nclosed | | Equipme | nt Design: | | | | |
| 36 | | Above Ground | | | | Compo | nent | | Mater | rial / Size / Rating / Other |
| 37 | | ✓ Stack M | ultiple Stack | | Burner | | | | | , |
| 38 | | Portable / Trailer | | | | Burner Tip / Assi | st Gas Rurner | _ | | 204/216 56 |
| 39 | | | | | | Burner E | | - | | 304/316 SS |
| 40 | Smokeless By: | Steam A | ssist Air | | Dilet | burner | Jouy | - | | Carbon Steel |
| 11 | | | taging | | Pilot | | | | | |
| 12 | | | wgiiig | | | Pilot T | ip | | | 304/316 SS |
| - 1 | Stack | [/] Colf Comment | | | | Pilot Lin | ie(s) | | | Carbon Steel |
| | Stack: | Self Supporting | | | Firebox / | Stack | | | | |
| H | Flare Burner: | | nokeless | Gas Assist | | Shel | I | | | NA |
| 15 | Pilot: | ✓ Intermittent ✓ | Continuous | | | Pipin | | | | |
| 16 | Pilot Air Inspirator: | ✓ Local | Remote | | | Nozzle | | - | | Carbon Steel |
| г | Pilot Flame Control: | No 🔽 | Yes (Thermo | ocounle) | | | | | | Carbon Steel |
| 18 | | Ľ | . es (memic | occupic) | | Flange | | | | Carbon Steel |
| ŀ | Pilot Ignition: | Flamefront Generator | Incoination | | | Insulati | | | | NA |
| H | r not ignition. | 7 -: | Inspirating I | | | Insulation | n Pins | | | NA |
| 0 | L | Electronic | Automatic | Manual | | Refract | огу | | | NA |
| 1 | | With Pilot Flame Control | | | | Refractory A | | | | NA NA |
| 2 | | With Auto Pilot Re-Ignition | | | | Ladders and F | | _ | | |
| 3 | | | | | | | | _ | | NA |
| 4 | Pilot Ignition Backup: | Manual Specify: i.e Pi | nzo Elast I | | | Stack Sample C | | | | NA |
| 5 | Г | | EZO-EIECTRIC | | | Sight GI | ass | | | NA |
| - | L | Battery Pack | | | | Othe | r | | | |

| ction: | UV Scanner | Ionization Rod | | s id Seal n Arrestor Off Valves ers er iransmitters | check w | 2 of B B 27 February JS SG MS LEED FABRICA Dual Head F NA |
|------------|--|--|--|--|--|---|
| ction: | Thermocouple UV Scanner Skid Mounted C Cor | P.O. No.: RFQ No.: Ref. P&ID Remarks: EQUIPME Ionization Rod | ENT SPECIFICATION Auxiliary Equipment Valves Blowers Dampers Inlet KO / Liqu Flame / Detonatio Instrumentation & Controls Solenoids / Shut- Flow Mete Calorimete Pressure Switches/T Thermocoup Temperature Switches BMS CEMS Other | Date: By: Checke Approv Supplie Model I s s sid Seal n Arrestor Off Valves err iransmitters oles | check w | 27 February JS SG MS SG MS LEED FABRICA Dual Head F NA |
| ction: | Thermocouple UV Scanner Skid Mounted C Cor | P.O. No.: RFQ No.: Ref. P&ID Remarks: EQUIPME Ionization Rod | ENT SPECIFICATION Auxiliary Equipment Valves Blowers Dampers Inlet KO / Liqu Flame / Detonatio Instrumentation & Controls Solenoids / Shut- Flow Mete Calorimete Pressure Switches/T Thermocoup Temperature Switches BMS CEMS Other | By: Checke Approv Supplie Model i s sid Seal n Arrestor Off Valves err iransmitters oles | red: Pr: No.: Check w | JS SG MS LEED FABRICA Dual Head F NA NA NA NA NA NA Yes with Sales for availa NA |
| ction: | Thermocouple UV Scanner Skid Mounted C Cor | RFQ No.: Ref. P&ID Remarks: EQUIPME Ionization Rod | ENT SPECIFICATION Auxiliary Equipment Valves Blowers Dampers Inlet KO / Liqu Flame / Detonatio Instrumentation & Controls Solenoids / Shut- Flow Mete Calorimete Pressure Switches/T Thermocoup Temperature Switches BMS CEMS Other | Checke Approv Supplie Model I Significant of the second | red: Pr: No.: Check w | SG MS LEED FABRICA Dual Head F NA NA NA NA NA NA NA Ves with Sales for availa NA |
| ction: | Thermocouple UV Scanner Skid Mounted ✓ Cor | Ref. P&ID Remarks: EQUIPME Ionization Rod | D: - ENT SPECIFICATION Auxiliary Equipment Valves Blowers Dampers Inlet KO / Liqu Flame / Detonatio Instrumentation & Controls Solenoids / Shut- Flow Mete Calorimete Pressure Switches/T Thermocoup Temperature Switches BMS CEMS Other | Supplie Model I Model I Significant Supplies S | Check w | NA NA NA NA NA NA NA NA NA Ves |
| ction: | UV Scanner Skid Mounted C Cor | Remarks: EQUIPME Ionization Rod | ENT SPECIFICATION Auxiliary Equipment Valves Blowers Damper: Inlet KO / Liqu Flame / Detonatio Instrumentation & Controls Solenoids / Shut-G Flow Mete Calorimete Pressure Switches/T Thermocoup Temperature Switches BMS CEMS Other | Model I | Check w | NA N |
| ction: | UV Scanner Skid Mounted C Cor | EQUIPME Ionization Rod FABRICATIO | Auxiliary Equipment Valves Blowers Damper: Inlet KO / Liqu Flame / Detonatio Instrumentation & Controls Solenoids / Shut-G Flow Mete Calorimet: Pressure Switches/T Thermocoup Temperature Switches BMS CEMS Other | Model I | Check w | NA NA NA NA Yes with Sales for availa NA |
| ction: | UV Scanner Skid Mounted C Cor | EQUIPME Ionization Rod FABRICATIO | Auxiliary Equipment Valves Blowers Damper: Inlet KO / Liqu Flame / Detonatio Instrumentation & Controls Solenoids / Shut-G Flow Mete Calorimet: Pressure Switches/T Thermocoup Temperature Switches BMS CEMS Other | sid Seal n Arrestor Off Valves ers er iransmitters | Check w | NA NA NA NA Yes vith Sales for availa NA NA NA vith Sales for availal NA |
| irements | UV Scanner Skid Mounted C Cor | FABRICATIO | Auxiliary Equipment Valves Blowers Damper: Inlet KO / Liqu Flame / Detonatio Instrumentation & Controls Solenoids / Shut-G Flow Mete Calorimet: Pressure Switches/T Thermocoup Temperature Switches BMS CEMS Other | s id Seal n Arrestor Off Valves ers er iransmitters | Check w | NA NA NA Yes vith Sales for availa NA NA NA vith Sales for availal NA vith Sales for availal NA |
| irements | UV Scanner Skid Mounted C Cor | FABRICATIO | Valves Blowers Damper: Inlet KO / Liqu Flame / Detonatio Instrumentation & Controls Solenoids / Shut-G Flow Mete Calorimet Pressure Switches/T Thermocoup Temperature Switches BMS CEMS Other | s id Seal n Arrestor Off Valves ers er iransmitters | Check w | NA NA NA Yes vith Sales for availa NA NA NA vith Sales for availal NA vith Sales for availal NA |
| irements [| Skid Mounted 🗸 Cor | | Blowers Damper: Inlet KO / Liqu Flame / Detonatio Instrumentation & Controls Solenoids / Shut-G Flow Mete Calorimet Pressure Switches/T Thermocoup Temperature Switches BMS CEMS Other | s id Seal n Arrestor Off Valves ers er iransmitters | Check w | NA NA NA Yes vith Sales for availa NA NA NA vith Sales for availal NA vith Sales for availal NA |
| irements [| | | Damper: Inlet KO / Liqu Flame / Detonatio Instrumentation & Controls Solenoids / Shut-C Flow Mete Calorimete Pressure Switches/T Thermocoup Temperature Switches BMS CEMS Other | s id Seal n Arrestor Off Valves ers er iransmitters | Check w | NA NA Yes vith Sales for availa NA NA NA vith Sales for availal NA vith Sales for availal NA |
| | | | Inlet KO / Liqu Flame / Detonatio Instrumentation & Controls Solenoids / Shut-C Flow Mete Calorimete Pressure Switches/T Thermocoup Temperature Switches BMS CEMS Other | id Seal n Arrestor Off Valves ers er iransmitters oles | Check w | NA Yes vith Sales for availa NA NA NA NA NA vith Sales for availal NA vith Sales for availal |
| | | | Flame / Detonatio Instrumentation & Controls Solenoids / Shut-C Flow Mete Calorimete Pressure Switches/T Thermocoup Temperature Switches BMS CEMS Other | n Arrestor Off Valves ers er iransmitters | Check w | Yes vith Sales for availa NA NA NA vith Sales for availal NA vith Sales for availal NA NA |
| | | | Instrumentation & Controls Solenoids / Shut-fow Mete Calorimete Pressure Switches/T Thermocoup Temperature Switches BMS CEMS Other | Off Valves ers er ransmitters | Check w | vith Sales for availa NA NA NA vith Sales for availal NA vith Sales for availal |
| | | | Solenoids / Shut-C Flow Mete Calorimete Pressure Switches/T Thermocoup Temperature Switches BMS CEMS Other | ers er ransmitters oles | Check w | NA NA NA vith Sales for availal NA vith Sales for availal |
| | | | Flow Mete Calorimetr Pressure Switches/T Thermocoup Temperature Switches BMS CEMS | ers er ransmitters oles | Check w | NA NA NA vith Sales for availal NA vith Sales for availal |
| | | | Calorimete Pressure Switches/T Thermocoup Temperature Switches BMS CEMS Other | er Fransmitters oles | | NA NA vith Sales for availal NA vith Sales for availal NA |
| | | | Pressure Switches/T Thermocoup Temperature Switches BMS CEMS Other | ransmitters oles | | NA vith Sales for availal NA vith Sales for availal NA |
| | | | Thermocou Temperature Switches BMS CEMS Other | oles | | vith Sales for availa NA vith Sales for availal NA |
| | | | Temperature Switches BMS CEMS Other | | | NA vith Sales for availal NA |
| | | | BMS CEMS Other | y i ansmitters | Check w | vith Sales for availal NA |
| | | | CEMS Other | | спеск w | NA |
| | | | Other | | | |
| | | | | | | NA NA |
| | | | ON AND INSPECTION | | | |
| | | | ON AND INSPECTION | | | |
| | | | ON AND INSPECTION | | | |
| | | | ON AND INSPECTION | | | |
| | | ncrete Pad | | | | |
| | Uther | | | Equipment | Info | |
| | | | Componer | nt | | Weight / Dimension |
| | ✓ Vendor Standard | | Burner | | | |
| 41f1 | Other. Specify: | | Burner Assen | nbly | | |
| tification | ✓ Vendor Standard | | Stack | 112 | | |
| | MTR | | Stack Assem | bly | | 8"OD x 10'H |
| | Certificate of Compliance | | Pilot Tip Pilot Line(s | 1 | | |
| | Other (Specify): | | Stack Assem | | | |
| | ✓ Vendor Standard | | Auxiliary Equipment | | | |
| | Radiography. Specify: | | Blowers | | | |
| | Ultrasonic. Specify: | | Inlet KO / Liquid | Seal | | |
| | Liquid Penetrant. | | Flame / Detonation | Arrestor | | |
| | | | Skid | | | |
| | | | Instrumentation & Controls | | | |
| aration [| | | BMS | | | |
| | | | Control Pan | el | | |
| - F | | | | | | |
| | 3 | | | | | |
| or _ | | | | | | |
| | Other. Specify: | | | | | |
| | | | | | | |
| | | | | | | |
| or | | Magnetic Particles. PMI. Specify: Other. Specify: Vendor Standard Other. Specify: Vendor Standard Other. Specify: Vendor Standard Other. Specify: Other. Specify: Other. Specify: | Magnetic Particles. PMI. Specify: Other. Specify: Vendor Standard Other. Specify: Vendor Standard Other. Specify: Vendor Standard Other. Specify: Other. Specify: Other. Specify: | Magnetic Particles. PMI. Specify: Other. Specify: Other. Specify: Other. Specify: Vendor Standard Other. Specify: Vendor Standard Other. Specify: Vendor Standard Other. Specify: Other. Specify: Other. Specify: Other. Specify: Other. Specify: | Magnetic Particles. PMI. Specify: Other. Specify: Other. Specify: Other. Specify: Other. Specify: Other. Specify: Vendor Standard Other. Specify: Vendor Standard Other. Specify: Vendor Standard Other. Specify: Other. Specify: Other. Specify: Other. Specify: | Magnetic Particles. Skid PMI. Specify: Instrumentation & Controls Other. Specify: Other. Specify: Other. Specify: Vendor Standard Other. Specify: Vendor Standard Other. Specify: Vendor Standard Other. Specify: Other. Specify: Other. Specify: Other. Specify: |

Van Buggenum 1-2H Item/Tag No.: Page of Project No.: Revision: В Date: 27 February 2014 Project: Ву: JS **Environmental Control Equipment** P.O. No.: Checked: SG Data Sheet RFQ No.: Approved: MS Client: Ref. P&ID: Site: Supplier: LEED FABRICATION Unit/Lease: Remarks: Model No.: **Dual Head Flare** GENERAL ARRANGEMENT **High Pressure** Low Pressure

| DEO | | Air Quality Divis | sion & ARQUALT | 71727 | | |
|---------------------------------------|--|--|---|-------------|--|--|
| WYOMING DEPARTMENT OF ENVIRONMENTAL | New Source Re | 50 Mary 10 Mar | tion Form Cover Sheet | | | |
| QUALITY | Is this a revision to an exist | | \$1505270211 | 36 | | |
| | Yes No | Date of Application | C/15/2015 | | | |
| | | Date of Application | on: 6/15/2015 | | | |
| Previous Application #: | | | | | | |
| COMPANY INFO | RMATION: | | | | | |
| Company Name: | | Peak Powder River R | Resources, LLC | | | |
| Address: | | 1910 Main Avenue | | | | |
| City: Dura | USA State: | | Zip Coo | le:81301 | | |
| | The second secon | Phone Number: | (970) 247-1500 | | | |
| FACILITY INFORM | MATION: | | | | | |
| New Facility or Existin | ng Engility: Now | Van Buggenur | m 1-2H | | | |
| Facility Description: | g Facility: New | Oil and Cas Duados | 41 - 5 - 111 | | | |
| Facility Class: | Minor | Oil and Gas Produc | | | | |
| Facility Type: | Production Site | Operating Status: C | perating | | | |
| For Oil & Gas Product | | | | | | |
| | on (FDOP)/Date of Modifica | ation: 3/24/2015 | | | | |
| Single well or multiple | | Single | | | | |
| Does production at th | is facility contain H2S?* | No | | | | |
| *If yes, contact the Di | | | | | | |
| API Number(s): | | 49-005 | 5-61581 | | | |
| NAICS Code: | | 2111 Oil and | Gas Extraction | | | |
| FACILITY LOCATION | | | | | | |
| *Enter the facility locatio | n in either the latitude/longitud | de area or section/township/ | range area. Both are not required. | | | |
| Physical Address: City: | | 7! 0 - 1 | | | | |
| State: WY | | Zip Code: | | | | |
| OR | County: | | | | | |
| Latitude: 43.737 | 7071 | 105 027422 | | | | |
| Quarter Quarter: | 7071 Longitude: SE | -105.837423 | | y: Campbell | | |
| Section: 35 | 4.7(7)30 | Quarter: 44N | SW | | | |
| 50.00.00.00.00.00.00 | | | Rang after the decimal (i.e. 41.12345, | e: 75W | | |
| CONTACT INFORM | MATION: | a coo r a a cam ana 5 argres | ajter the decimal (i.e. 41.12345, | -107.56789) | | |
| | AND NSR Permitting Contact is require | ed for your application to be doom | od somplete by the | | | |
| Title: Ms. | First Name: | ed for your application to be deemi | Daneka | | | |
| Last Name: | Ewert | | Darieka | _ | | |
| Company Name: | | Peak Powder River Re | esources. LLC | | | |
| Job Title: | | Environmental Manag | | | | |
| Address: | | 1910 Main Avenue | | | | |
| | | State: | Colorado | | | |
| 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 | 81301 | | | _ | | |
| Primary Phone No.: | (307) 231-0755 | E-mail: | DEwert@colopeaks | .com | | |
| Mobile Phone No.: | Factoria 1 | Fax No.: | (970) 247-5424 | 1 | | |
| Contact Type: | Environmental contact | Start Date: | | | | |
| *Name of the contact | to whom the permit will be | issued: | | | | |

| Additional Contact Ty | pe (if needed): | Environment | alcontact | | |
|--|-----------------------|-----------------------|-------------------|-------------------------|----------------------|
| Title: Ms. | First Nar | | ai contact | Daneka | |
| Last Name: | - | wert | | рапека | |
| Company Name: | | | k Powder River | Resources IIC | |
| Job Title: | | Envir | onmental Mana | ager | |
| Address: | | | 10 Main Avenu | | |
| City: | Durango | State: | | Colorado | |
| Zip Code: | 81301 | | | colorado | |
| Primary Phone No.: | (307) 231-07 | ' 55 | E-mail: | DFwei | rt@colopeaks.com |
| Mobile Phone No.: | | | Fax No.: | | 970) 247-5424 |
| Contact Type: | Environmental o | | Start Date: | ,- | 7.07 217 3121 |
| FACILITY APPLICA | ATION INFORM | ATION: | | | |
| General Info: | | | | | |
| Has the facility change | d location or is it a | new/ greenfield fa | acility? | | Yes |
| Has a Land Use Plannir | ng document been | included in this ap | plication? | | No |
| Is the facility located in | n a sage grouse cor | e area?* | | | No |
| If the facility is in a sag | e grouse core area | , what is the WER i | number? | | |
| * For questions about | sage grouse core a | rea, contact WY Go | ame & Fish Dep | artment. | |
| Federal Rules App | olicability - Fac | ility Level: | | | |
| Prevention of Significa | nt Deterioration (P | SD): | | | No |
| Non-Attainment New S | | | | | No |
| Modeling Section | : | | | | NO |
| Has the Air Quality Div | | ed to determine if | modeling is requ | uired? | No |
| Is a modeling analysis p | part of this applicat | ion? | modeling is requ | uneur | No No |
| Is the proposed project | subject to Prevent | ion of Significant I | Deterioration (D | SD) roquiroments? | N |
| Has the Air Quality Divi | sion been notified | to schedule a pre- | application mee | sting? | No |
| Has a modeling protoco | ol been submitted | to and approved by | the Air Ouality | , Division3 | No |
| Has the Air Quality Divi | sion received a Q/I | O analysis to submi | it to the respect | ive El Ms to dotormin | No |
| the need for an AQRV a | nalysis? | arranyono to Submi | ic to the respect | ive ruvis to determin | |
| Required Attachm | | | | | No |
| Facility Map | | | | | |
| Process Flow Diagram | | □ ☑ | | | |
| Modeling Analysis (if ap | oplicable) | | | | |
| Land Use Planning Docu | | | | | |
| Detailed Project Descrip | | <u> </u> | | | |
| Emissions Calculations | | <u> </u> | | | |
| | | | | | |
| l, | | Ewert | | Environmer | ntal Manager |
| | Kesponsible Offic | ial (Printed Name) | | | itle |
| | | | | | |
| an Official Barress Lui | 6.1 | | | | |
| an Official Representati | ve of the Company | , state that I have I | knowledge of th | ne facts herein set for | th and that the same |
| are true and correct to t and emission rates listed | the best of my know | wledge and belief. | I further certify | that the operational | information provided |

application reflect the anticipated emissions due to the operation of this facility. The facility will operate in compliance with all applicable Wyoming Air Quality Standards and Regulations.

Signature: Cynthia Mades on (ink) for Daneka Ewerf

Date: June 12 2012

Separator/Treater

| Company Equipment ID: 2-Phase Sepa Company Equipment Description: | | parator | | | | |
|--|---|--|--|--|--|--|
| | | 2-Phase Separator | | | | |
| | | | | | | |
| Operating Status: Operating | | | | | | |
| Initial Construction Commencem | | | | | | |
| Initial Operation Commencement | t Date: | 3/18/2015 | | | | |
| Most Recent Construction/ Modi | fication | | | | | |
| Commencement Date: | | | | | | |
| | | | | | | |
| Most Recent Operation Commen | cement Date: | | | | | |
| Select reason(s) for this emission | s unit being i | included in this application (must be completed regardless of date | | | | |
| of installation or modification): | Ü | thust be completed regardless of date | | | | |
| Reason: Constructi | on (Greenfield | d/New Facility) | | | | |
| | • | , | | | | |
| If reason is <i>Reconstruction</i> or <i>Ter</i> | mporary Perm | nit or Other, please explain below: | | | | |
| | | produce explain below. | | | | |
| | | | | | | |
| | | | | | | |
| Type of Vessel: 2-Phase | Separator | Is Vessel Heated? No | | | | |
| Operating Temperature (F): | 80 | 110 | | | | |
| Operating Pressure (psig): | 100 | | | | | |
| | | | | | | |
| SCC Codes: List all Source Classific | ation Code(s) | (SCC) that describe the process(es) performed by the emission | | | | |
| source (e.g., 1-02-002-04). | • | , was a second the process(es) performed by the emission | | | | |
| | | | | | | |
| 31000107 | | | | | | |
| | | | | | | |
| Potential Operating Schedule: | Provide the o | perating schedule for this emission unit. | | | | |
| | 24 | | | | | |
| Hours/year: | 8760 | | | | | |
| | | | | | | |

| Control Equipment: No |
|---|
| If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets. |
| |
| Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit? |
| ☐ Yes ☑ No |
| Pollutant: |
| Proposed BACT: |
| *If yes, attach BACT Analysis with this application. |
| |
| Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit? |
| ☐ Yes ☑ No |
| Pollutant: |
| Proposed LAER: |
| *If yes, attach LAER Analysis with this application. |
| Endaral and State Bule Applicability |
| Federal and State Rule Applicability: New Source Performance Standards (NSPS): Subject, but exempt |
| |
| New Source Performance Standard are listed under 40 CFR 60- |
| Standards of Performance for New Stationary Sources. |
| NSPS Subpart: 0000 |
| National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61): Not Affected |
| National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR |
| 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride). |
| Part 61 NESHAP Subpart: |
| |
| National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63): Not Affected |
| National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) |
| standards are listed under 40 CFR 63 |
| Part 63 NESHAP Subpart: |
| |
| Prevention of Significant Deterioration (PSD): Not Affected |
| These rules are found under WAQSR Chapter 6, Section 4. |
| Non Attainment No. C |
| Non-Attainment New Source Review: Not Affected |
| These rules are found under WAQSR Chapter 6, Section 13. |

Separator/Treater

| Company Equipment ID: | Treater |
|--|---|
| Company Equipment Description: | Treater |
| | |
| Operating Status: Operating | |
| Initial Construction Commencemer | |
| Initial Operation Commencement D | |
| Most Recent Construction/ Modific | cation |
| Commencement Date: | |
| | |
| Most Recent Operation Commence | |
| | unit being included in this application (must be completed regardless of date |
| of installation or modification): | |
| Reason: Construction | n (Greenfield/New Facility) |
| | |
| If reason is <i>Reconstruction</i> or <i>Tem</i> | porary Permit or Other, please explain below: |
| | |
| | |
| T . ()/ | |
| | Treater Is Vessel Heated? Yes |
| | 130 |
| Operating Pressure (psig): | 30 |
| | |
| | tion Code(s) (SCC) that describe the process(es) performed by the emission |
| source (e.g., 1-02-002-04). | |
| | 242242 |
| | 31000107 |
| Potential Operating Schedule: | Provide the operating schedule for this emission unit. |
| 100 | 24 |
| - | 3760 |
| Hours/year. | 37.00 |

| Control Equipment: No If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets. |
|--|
| Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit? Yes No Pollutant: Proposed BACT: |
| *If yes, attach BACT Analysis with this application. |
| Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit? Yes No Pollutant: |
| Proposed LAER: |
| *If yes, attach LAER Analysis with this application. |
| Federal and State Rule Applicability: New Source Performance Standards (NSPS): Subject, but exempt New Source Performance Standard are listed under 40 CFR 60- Standards of Performance for New Stationary Sources. NSPS Subpart: OOOO |
| National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61): Not Affected |
| National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride). Part 61 NESHAP Subpart: |
| National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63): Not Affected |
| National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63 Part 63 NESHAP Subpart: |
| Prevention of Significant Deterioration (PSD): Not Affected These rules are found under WAQSR Chapter 6, Section 4. |
| Non-Attainment New Source Review: Not Affected These rules are found under WAQSR Chapter 6, Section 13. |

Storage Tank/Silo

| Company Equipment ID: | Oil Tanks | | | | | |
|--|------------------|------------------|------------|---------------|-------------|------------------------|
| Company Equipment Description | | 4 400-BBL C | il Tanks | | | |
| | | | | | | |
| Operating Status: Operating | | | | | | |
| Initial Construction Commenceme | | | | | | |
| Initial Operation Commencement | | | 3/1 | .8/2015 | | |
| Most Recent Construction/ Modif | fication | | | | | _ |
| Commencement Date: | | | | | | |
| Most Posent Operation Commun. | | | | | | |
| Most Recent Operation Commend | | ما الماما الماما | | / | | - |
| Select reason(s) for this emission of installation or modification): | is unit being if | nciuaea in th | is applica | ation (must | be comple | ted regardless of date |
| Reason: Construction | on (Groonfield | I/Now Facility | .\ | 7 | | |
| Reason. Construction | on (Greenheid | i/New Facility | () | | | |
| If reason is <i>Reconstruction</i> or <i>Ter</i> | nnorary Perm | it or Other | nloaco o | سواما مامس | | |
| The second secon | iiporary r eriii | it of other, | piease ex | kpiairi below | • | |
| | | | | | | |
| | | | | | | |
| Material Type: Liquid | 1 | | | | | |
| Description of Material Stored: | 1 | 36 deg API c | il | | | |
| | | | | | | |
| Capacity: 1600 | | l | Jnits: | barrels | | |
| Maximum Throughput: | 214 | | | | ם Units: | barrels/day |
| Maximum Hourly Throughput: | 9 | | | | Units: | barrels/hr |
| Operating Pressure (psig): | 0 | | | _ | | |
| Vapor Pressure of Material Stored | (psig): | 3.5 | | | - | |
| Is Tank Heated?: No | | | | | - | |
| | | | | | | |
| SCC Codes: List all Source Classific | ation Code(s) | (SCC) that de | scribe th | e process(es |) performe | ed by the emission |
| source (e.g., 1-02-002-04). | | | | | | |
| | | | | | | |
| | | 404003 | 12 | | | |
| Potential Operating Sahadala | Describe of | | | | | |
| | Provide the o | perating sch | edule for | this emissio | n unit. | |
| Hours/day: Hours/year: | 24 | | | _ | | |
| riours/year. | 8760 | | | _ | | |

| Control Equipment: No |
|---|
| If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets. |
| |
| Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit? |
| □ Yes ☑ No |
| Pollutant: |
| Proposed BACT: |
| *If yes, attach BACT Analysis with this application. |
| Town ATT - U. Town |
| Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit? |
| ☐ Yes ☑ No |
| Pollutant: |
| Proposed LAER: |
| *If yes, attach LAER Analysis with this application. |
| Fodoral and State Bule Applicability |
| Federal and State Rule Applicability: New Source Porformance Standards (NSPS) |
| New Source Performance Standards (NSPS): Subject, but exempt |
| New Source Performance Standard are listed under 40 CFR 60- |
| Standards of Performance for New Stationary Sources. |
| NSPS Subpart: 0000 |
| National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61): Not Affected |
| National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61): Not Affected |
| National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride). |
| Part 61 NESHAP Subpart: |
| |
| National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63): Not Affected |
| National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63): National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) otendards are Vista de la 1000 Financia (NESHAP Part 63) |
| standards are listed under 40 CFR 63 |
| Part 63 NESHAP Subpart: |
| |
| Prevention of Significant Deterioration (PSD): Not Affected |
| These rules are found under WAQSR Chapter 6, Section 4. |
| |
| Non-Attainment New Source Review: Not Affected |
| These rules are found under WAQSR Chapter 6, Section 13. |
| process Control of the Control of t |

Storage Tank/Silo

| Company Equipment ID: | Water Tank | | | | |
|---|-----------------|-------------------------|---------------|-------------|-----------------------------|
| Company Equipment Description | n: | 400-BBL Produced \ | Nater Tank | | |
| | | | | | |
| Operating Status: Operating | | | | | |
| Initial Construction Commencer | nent Date: | | | | |
| Initial Operation Commencemen | ıt Date: | 3/ | 18/2015 | | |
| Most Recent Construction/ Mod | ification | | | | - |
| Commencement Date: | | | | | |
| | | | | | |
| Most Recent Operation Commer | ncement Date: | | | | |
| Select reason(s) for this emissio | ns unit being i | ncluded in this applic | cation (must | be comple | — ted regardless of date |
| of installation or modification): | 1540 | | | | and a spar areas of date |
| Reason: Construct | ion (Greenfield | d/New Facility) | | | |
| | | | | | |
| If reason is <i>Reconstruction</i> or <i>Te</i> | mporary Perm | nit or Other, please e | explain below | /: | |
| | | | • | | |
| | | | | | |
| | _ | | | | |
| Material Type: Liquid | | | | | |
| Description of Material Stored: | | Produced Water | | | |
| | | | | | |
| Capacity: 400 | | Units: | barrels | | |
| Maximum Throughput: | 200 | | | Units: | barrels/day |
| Maximum Hourly Throughput: | 21 | | | Units: | barrels/hr |
| Operating Pressure (psig): | 0 | | | | |
| Vapor Pressure of Material Store | d (psig): | 0.178 | | _ | |
| Is Tank Heated?: No | | | | _ | |
| | | | | | |
| SCC Codes: List all Source Classific | cation Code(s) | (SCC) that describe the | ne process(e | s) performe | ed by the emission |
| source (e.g., 1-02-002-04). | | | | | |
| | | | | | |
| | | 40400312 | | | |
| | | | | | |
| Potential Operating Schedule: | Provide the o | perating schedule for | this emissic | n unit. | |
| Hours/day: | 24 | | _ | | |
| Hours/year: | 8760 | | | | |
| | | | | | |

| Control Equipment: No |
|--|
| If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets. |
| I works neets. |
| Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit? |
| ⊔ Yes ☑ No |
| Pollutant: |
| Proposed BACT: |
| *If yes, attach BACT Analysis with this application. |
| |
| Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit? |
| ⊔ Yes ☑ No |
| Pollutant: |
| Proposed LAER: |
| *If yes, attach LAER Analysis with this application. |
| Fordered and Color D. L. A. H. L. W. |
| Federal and State Rule Applicability: |
| New Source Performance Standards (NSPS): Subject, but exempt |
| New Source Performance Standard are listed under 40 CFR 60- |
| Standards of Performance for New Stationary Sources. |
| NSPS Subpart: 0000 |
| National Emission Standards for Hazarday, At B. H (2) |
| National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61): Not Affected |
| National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR |
| 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride). Part 61 NESHAP Subpart: |
| art of NESHAP Subpart: |
| National Emission Standards for Hazardous Air Ballyton L. (N. Sauce Co.) |
| National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63): Not Affected |
| National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63 |
| Part 63 NESHAP Subpart: |
| art 05 NESTIAF Subpart. |
| Prevention of Significant Deterioration (PSD): |
| These rules are found under WAQSR Chapter 6, Section 4. |
| |
| Non-Attainment New Source Review: Not Affected |
| These rules are found under WAQSR Chapter 6, Section 13. |
| Section 13. |

Loading/Unloading/Dump

| Company Equipment ID: Truckloading | | |
|---|--|-------------------------|
| Company Equipment Description: | Truckloading | |
| | | |
| Operating Status: Operating | | |
| Initial Construction Commencement Date: | | |
| Initial Operation Commencement Date: | 3/18/2014 | - |
| Most Recent Construction/ Modification | | - |
| Commencement Date: | | |
| | | - |
| Most Recent Operation Commencement Date: | | |
| Select reason(s) for this emissions unit being in | ncluded in this application (must be completed | d regardless of date of |
| installation or modification): | | |
| Reason: Construction (Greenfield | d/New Facility) | |
| | | |
| If reason is Reconstruction or Temporary Perm | nit or Other, please explain below: | |
| | | |
| | | |
| Torre of Market 1 | | |
| Type of Material: Liquid | | |
| Material Description: Crude Oil | | |
| Maximum Annual Throughput: 78,110 | H-4 | I / |
| Maximum Hourly Throughput: 78,110 | Units: | barrels/yr |
| Detailed Description of Loading/Unloading/Dun | Units: | barrels/hr |
| submerged loading, dedicated service from oil s | | |
| | storage tarks to 180-BBE truck tark | |
| | | |
| SCC Codes: List all Source Classification Code(s) | (SCC) that describe the process(es) performed | hy the emission source |
| (e.g., 1-02-002-04). | , , , , , , , , , , , , , , , , , , , | by the emission source |
| | | |
| | 40600132 | |
| | | |
| Potential Operating Schedule: Provide the o | operating schedule for this emission unit. | |
| Hours/day: 2 | | |
| Hours/year: 434 | | |
| | | |

| Control Equipment: No | |
|---|--------------------------|
| If yes, please fill out and attach the appropriate Control Device and Release Point Information | tion worksheets |
| | non worksheets. |
| Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission | n unit? |
| □ Yes ☑ No | |
| Pollutant: | |
| Proposed BACT: | |
| *If yes, attach BACT Analysis with this application. | |
| Laurent Aultzweit I. P. J. J. Bur Grand | |
| Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission | unit? |
| ☐ Yes ☑ No Pollutant: | |
| Proposed LAER: | |
| *If yes, attach LAER Analysis with this application. | |
| if yes, attach EAEN Analysis with this application. | |
| Federal and State Rule Applicability: | |
| Ni. Company | |
| New Source Performance Standards (NSPS): Subject, but exempt New Source Performance Standard are listed under 40 CFR 60- | |
| Standards of Performance for New Stationary Sources. | |
| NSPS Subpart: 0000 | |
| | |
| National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61): | Not Affected |
| National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are | listed under 40 CED 64 |
| (These include asbestos, benzene, beryllium, mercury, and vinyl chloride). | iisted diidei 40 CFR 61. |
| Part 61 NESHAP Subpart: | |
| | |
| National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63): | Not Affected |
| National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) | |
| standards are listed under 40 CFR 63 | |
| Part 63 NESHAP Subpart: | |
| Provention of Significant Details (PSD) | _ |
| Prevention of Significant Deterioration (PSD): Not Affected Those rules are found under WACOB Classes. | |
| These rules are found under WAQSR Chapter 6, Section 4. | |
| Non-Attainment New Source Review: Not Affected | |
| These rules are found under WAQSR Chapter 6, Section 13. | |
| are really and thingon onapier o, deciron 13. | |

Fugitives

| Company Equipment ID: Fu | gitives |
|--|---|
| Company Equipment Description: | Fugitives |
| Operating Status: Operating | |
| Operating Status: Operating | |
| Initial Construction Commencement | |
| Initial Operation Commencement Da | |
| Most Recent Construction/ Modificat | ion |
| Commencement Date: | |
| | |
| Most Recent Operation Commencem | ient Date: |
| Select reason(s) for this emissions un | nit being included in this application (must be completed regardless of date of |
| installation or modification): | |
| Reason: Construction (| Greenfield/New Facility) |
| | , |
| If reason is Reconstruction or Tempo | prary Permit or Other, please explain below: |
| casen is necessariation of rempe | wary retrine of Other, please explain below. |
| | |
| | |
| Type of Fugitive Emission: | gitive Leaks at O&G |
| Type of Tugitive Emission. | grive Leaks at O&O |
| SCC Codes: List all Course Classification | 0.1.4 \ \ (0.00) \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ |
| | on Code(s) (SCC) that describe the process(es) performed by the emission |
| source (e.g., 1-02-002-04). | |
| | |
| | 31000101 |
| Paradial Occupies O. I. I | |
| | ovide the operating schedule for this emission unit. |
| Hours/day: 24 | |
| Hours/year: 87 | 60 |
| | |

| Control Equipment: No If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets. |
|--|
| Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit? Yes No Pollutant: Proposed BACT: |
| *If yes, attach BACT Analysis with this application. |
| Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit? Yes No Pollutant: |
| Proposed LAER: *If yes, attach LAER Analysis with this application. |
| Federal and State Rule Applicability: New Source Performance Standards (NSPS): Subject, but exempt New Source Performance Standard are listed under 40 CFR 60- Standards of Performance for New Stationary Sources. NSPS Subpart: OOOO |
| National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61): Not Affected |
| National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride). Part 61 NESHAP Subpart: |
| National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63): Not Affected |
| National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63 Part 63 NESHAP Subpart: |
| Prevention of Significant Deterioration (PSD): Not Affected These rules are found under WAQSR Chapter 6, Section 4. |
| Non-Attainment New Source Review: Not Affected These rules are found under WAQSR Chapter 6, Section 13. |

Control Equipment:

Flare/Combustor

| Manufacturer: | LEED | | | | Date | Installed: | 3/1/20 |)15 |
|---------------------------------------|--------------|---------------------|---------|------------------------|--------------|--|---------|------------|
| Model Name and | | | | | Comp | any Control | | |
| Number: | L30-0011 | | | | | ment ID: | | |
| Company Control Equ | uipment | | | | | | | |
| Description: | | 48-IN by 25 | 5-FT Sm | okeless Combus | tor | | | |
| Pollutant(s) Controlle PM (FIL) Other | | □ CO Condensible | □ NC | Ox ☐ Pb PM 10 (FIL) | □ So | O2 ☑ VOC PM 2.5 (FIL) | _ | 1 PM 2.5 |
| NOTE: The following | fields requi | re numeric | values | unless otherwis | se den | oted with an aster | isk* | |
| Maximum Design Cap | acity (MMS | CF/hr): | 0.004 | | | | | |
| Minimum Design Cap | acity (MMSC | CF/hr): | 0 | | | | - | |
| Design Control Efficie | ncy (%): | 98 | | Capture Ef | ficienc | y (%): | 100 | |
| Operating Control Eff | iciency (%): | | 98 | | | | | |
| Flare Type:* | Enclosed | | | Elevated F | - lare Ty | pe:* Non-A | ssisted | |
| Ignition Device:* | Yes | | • | Flame Prese | | The second secon | | |
| Inlet Gas Temp (F): | 100 | | | | Flame | e Presence Type:* | Th | ermocouple |
| Gas Flow Rate (acfm): | | 0 | .7 | | Outlet | t Gas Temp (F): | 1000 | |
| This is the | only control | equipment | on thi | s air contaminan | nt sour | ce | | |
| If not, this control equ | uipment is: | | | Primary | | Secondary | | Parallel |
| List all other emission | units that a | are also | | ţ. | | , | | |
| vented to this contro | l equipment | * | none | | | | | |
| List all release point I | | | | | | | | |
| this control equipmen | nt:* | | none | | | | | |
| | | | | | | | | |

OIL TANKS

Emissions Information- The following tables request information needed to determine the applicable requirements and the compliance status of this emission unit with those requirements.

| | | | Effi | ciency Standards | 1 | | |
|-----------|--|----------------------------------|------------------|----------------------|---------------------|----------------------|---------------|
| | | Pre-Controlled | Potential | T | Potential | Potential | T |
| | | Potential Emissions (tons/yr) | to Emit (PTE) | Units | to Emit (lbs/hr) | to Emit (tons/yr) | Basis for |
| iteria Po | llutants: | (10113/ 41/ | (1 1 2) | Offics | (103/111) | (toris/yr) | Determination |
| 1.) | | T | T | | | | T |
| 1., | Particulate emissions (PE/PM) (formerly particulate matter, PM) | | | | | | |
| 2.) | PM #10 microns in diameter (PE/PM10) | | | | | | |
| 3.) | | | | | | | |
| 4.) | Sulfur dioxide (SO2) | | | | | | |
| | Nitrogen Oxides (NOx) | | | | | | |
| 6.) | Carbon monoxide (CO) | | | | | | 2 |
| • | Volatile organic compounds (VOC) | 5.56 | 1.043935 | lb/ton of production | 1.269406 | 5.56 | Tanks Program |
| 8.) | Lead (Pb) | | | | | | |
| | Total Hazardous Air Pollutants (HAPs) | 0.09 | 0.016898 | lb/ton of production | 0.020548 | 0.09 | Tanks Program |
| 10.) | Fluoride (F) | | | | | | |
| 11.) | Hydrogen Sulfide (H2S) | | | | | | |
| 12.) | Mercury (Hg) | | | | | | |
| 13.) | Total Reduced Sulfur (TRS) | | | | | | |
| 14.) | Sulfuric Acid Mist (SAM) | | | | | | |

^{*}Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

SHANNON oil weighs 6.494 LB/GAL (42 GAL/BBL) = 272.75 LB/BBL Projected oil production = 78,110 BBL 272.75 LB/BBL (78,110 BBL) (78,110

BURNER

Emissions Information- The following tables request information needed to determine the applicable requirements and the compliance status of this emission unit with those requirements.

| • | | statas of this cirristion | Commence of the local division in the local | ciency Standards | 1 | | |
|-------------|--|----------------------------------|---|----------------------|---------------------|----------------------|---------------|
| | | Pre-Controlled | Potential | | Potential | Potential | T |
| | | Potential Emissions (tons/yr) | to Emit (PTE) | Units | to Emit (lbs/hr) | to Emit (tons/yr) | Basis for |
| Criteria Po | llutants | (10113/ 91) | (1 1 1) | Units | (105/111) | (toris/yr) | Determination |
| 1.) | | T | T | T | _ | | |
| 1.) | Particulate emissions (PE/PM) (formerly particulate matter, PM) | | | | | | |
| 2.) | PM #10 microns in diameter (PE/PM10) | | | | | | |
| 3.) | PM #2.5 microns in diameter (PE/PM2.5) | | | | | | |
| 4.) | Sulfur dioxide (SO2) | | | | | | |
| 5.) | Nitrogen Oxides (NOx) | 0.28 | 0.052572 | lb/ton of production | 0.063927 | 0.28 | AP-42 |
| 6.) | Carbon monoxide (CO) | 0.23 | 0.043184 | lb/ton of production | 0.052511 | 0.23 | AP-42 |
| 7.) | Volatile organic compounds (VOC) | | | | | | |
| 8.) | Lead (Pb) | | | | | | |
| 9.) | Total Hazardous Air Pollutants (HAPs) | | | | | | |
| 10.) | Fluoride (F) | | | | | | |
| 11.) | Hydrogen Sulfide (H2S) | | | | | | |
| 12.) | Mercury (Hg) | | | | | | |
| 13.) | Total Reduced Sulfur (TRS) | | | | | | |
| 14.) | Sulfuric Acid Mist (SAM) | | | | | | |

^{*}Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

SHANNON oil weighs 6.494 LB/GAL (42 GAL/BBL) = 272.75 LB/BBL Projected oil production = 78,110 BBL 272.75 LB/BBL (78,110 BBL) (TON/2000 LB) = 10,652 TONS oil/yr. LB/TON of production = X TON / 10,652 TONS (2000 LB/TON) LB/HR = X TONS/8760 HR (2000 LB/TON)

FUGITIVES

Emissions Information- The following tables request information needed to determine the applicable requirements and the compliance status of this emission unit with those requirements.

| | | | Efficiency Standards | | 1 | | |
|-------------|--|--|-------------------------------|----------------------|----------------------------------|-----------------------------------|----------------------------|
| | | Pre-Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE) | Units | Potential to Emit (lbs/hr) | Potential to Emit (tons/yr) | Basis for Determination |
| Criteria Po | llutants: | | | | | | |
| 1.) | Particulate emissions (PE/PM) (formerly particulate matter, PM) | | | | | | |
| 2.) | PM #10 microns in diameter (PE/PM10) | | | | | | |
| 3.) | PM #2.5 microns in diameter (PE/PM2.5) | | | | | | |
| | Sulfur dioxide (SO2) | | | | | | |
| 5.) | Nitrogen Oxides (NOx) | | | | | | |
| 6.) | Carbon monoxide (CO) | | | | | | |
| 7.) | Volatile organic compounds (VOC) | 0.14 | 0.026286 | lb/ton of production | 0.031963 | 0.14 | AP-42 |
| 8.) | Lead (Pb) | | | | | | |
| 9.) | Total Hazardous Air Pollutants (HAPs) | 0.10 | 0.018776 | lb/ton of production | 0.022831 | 0.10 | AP-42 |
| | Fluoride (F) | | | | | | |
| 11.) | Hydrogen Sulfide (H2S) | | | | | | |
| 12.) | Mercury (Hg) | | | | | | |
| 13.) | Total Reduced Sulfur (TRS) | | | | | | |
| | Sulfuric Acid Mist (SAM) | | | | | | |

^{*}Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

SHANNON oil weighs 6.494 LB/GAL (42 GAL/BBL) = 272.75 LB/BBL Projected oil production = 78,110 BBL 272.75 LB/BBL (78,110 BBL) (TON/2000 LB) = 10,652 TONS oil/yr. LB/TON of production = X TON / 10,652 TONS (2000 LB/TON) LB/HR = X TONS/8760 HR (2000 LB/TON)

Truck Loading

Emissions Information- The following tables request information needed to determine the applicable requirements and the compliance status of this emission unit with those requirements.

| | • | | Control of the Contro | ciency Standards | 1 | | |
|---------|--|---------------------------------------|--|----------------------|----------------------|----------------------|---------------|
| | | Pre-Controlled Potential Emissions | Potential to Emit | | Potential to Emit | Potential to Emit | Basis for |
| eria Po | ollutants: | (tons/yr) | (PTE) | Units | (lbs/hr) | (tons/yr) | Determination |
| 1.) | | I | T | | T | T | Γ |
| | Particulate emissions (PE/PM) (formerly particulate matter, PM) | | | | | | |
| 2.) | PM #10 microns in diameter (PE/PM10) | | | | | | |
| 3.) | PM #2.5 microns in diameter (PE/PM2.5) | | | | | | |
| 4.) | Sulfur dioxide (SO2) | | | | | | |
| 5.) | Nitrogen Oxides (NOx) | | | | | | |
| 6.) | Carbon monoxide (CO) | | | | | | |
| 7.) | Volatile organic compounds (VOC) | 0.98 | 0.184003 | lb/ton of production | 0.223744 | 0.98 | AP-42 |
| 8.) | Lead (Pb) | | | | | | |
| 9.) | Total Hazardous Air Pollutants (HAPs) | 0.01 | 0.001878 | lb/ton of production | 0.002283 | 0.01 | AP-42 |
| | Fluoride (F) | | | | | | |
| 11.) | Hydrogen Sulfide (H2S) | | | | | | |
| 12.) | Mercury (Hg) | | | | | | |
| 13.) | Total Reduced Sulfur (TRS) | | | | | | |
| 14.) | Sulfuric Acid Mist (SAM) | | | | | | |

^{*}Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

SHANNON oil weighs 6.494 LB/GAL (42 GAL/BBL) = 272.75 LB/BBL Projected oil production = 78,110 BBL 272.75 LB/BBL (78,110 BBL) (TON/2000 LB) = 10,652 TONS oil/yr. LB/TON of production = X TON / 10,652 TONS (2000 LB/TON) LB/HR = X TONS/8760 HR (2000 LB/TON)

Complete the table below for *each* release point. Please include release point information for each emission unit. Multiple attachments may be necessary. A release point is a point at which emissions from an emission unit are released into the ambient (outside)air. List each individual release point on a separate pair of lines (release point ID and description). *For longitude and latitude, use NAD 83/WGS84 datum and 5 digits after the decimal* (i.e. 41.12345, -107.56789)

| Stack Release Point Information | | | | | | |
|--|----------------------------|-------------|--|--|--|--|
| Company Release Point ID: | Release Point Type: Ver | tical | | | | |
| OIL TANKS - WITH COMBUSTOR | Release Point Latitude: | 43.737071 | | | | |
| | Release Point Longitude: | -105.837423 | | | | |
| Company Release Point Description: | Base Elevation (ft): 530 | | | | | |
| vapors from oil tanks routed to 48-IN by 25- | Stack Height (ft): 20 | | | | | |
| FT combustor | Stack Diameter (ft): 4 | | | | | |
| | Exit Gas Velocity (ft/s): | 0.01 | | | | |
| | Exit Gas Temp (F): 100 | 00 | | | | |
| | Exit Gas Flow Rate (acfm): | 0.7 | | | | |
| Company Release Point ID: | Release Point Type: Hor | rizontal | | | | |
| OIL TANKS - NO CONTROL | Release Point Latitude: | 43.737071 | | | | |
| | Release Point Longitude: | -105.837423 | | | | |
| Company Release Point Description: | Base Elevation (ft): 530 | 03 | | | | |
| vapors exit 4-inch tank vent pipe | Stack Height (ft): 20 | | | | | |
| | Stack Diameter (ft): 0.8 | 3 | | | | |
| | Exit Gas Velocity (ft/s): | 0.01 | | | | |
| | Exit Gas Temp (F): 100 | 00 | | | | |
| | Exit Gas Flow Rate (acfm): | 0.7 | | | | |
| Company Release Point ID: | | tical | | | | |
| 0.5 MMBTU/HR TREATER BURNER | Release Point Latitude: | 43.737071 | | | | |
| | Release Point Longitude: | -105.837423 | | | | |
| Company Release Point Description: | Base Elevation (ft): 530 |)3 | | | | |
| fumes from the combustion of natural gas | Stack Height (ft): 20 | | | | | |
| exiting the burner stack | Stack Diameter (ft): 0.8 | 3 | | | | |
| | Exit Gas Velocity (ft/s): | 0.01 | | | | |
| | Exit Gas Temp (F): 100 | | | | | |
| | Exit Gas Flow Rate (acfm): | 6.2 | | | | |
| Company Release Point ID: | | rizontal | | | | |
| TRUCK LOADING | Release Point Latitude: | 43.737071 | | | | |
| | Release Point Longitude: | -105.837423 | | | | |
| Company Release Point Description: | Base Elevation (ft): 530 |)3 | | | | |
| vapors displaced from truck tank as oil is | Stack Height (ft): 12 | | | | | |
| loaded into tank | Stack Diameter (ft): 0.83 | 3 | | | | |
| | Exit Gas Velocity (ft/s): | 0.01 | | | | |
| | Exit Gas Temp (F): 50 | | | | | |
| | Exit Gas Flow Rate (acfm): | 16.83 | | | | |

Tanks: ACFM = (MSCF/DAY) (1000 SCF/MCF) (DAY/24 HR) (HR/60 MIN)Burners: $ACFM = (MMBTU/HR)(HR/60 MIN)(SCF/BTU)(10^6 BTU/MMBTU)$ Truckloading: (180 BBL/HR)(HR/60 MIN)(5.61 CF/BBL) = 16.83 ACFM

| Company Release Point ID: | Dologgo Daint Tura | |
|------------------------------------|----------------------------|-------------|
| Company Release Point ID. | Release Point Type: | |
| | Release Point Latitude: | |
| Common Pologo Pologo | Release Point Longitude: | |
| Company Release Point Description: | Base Elevation (ft): | |
| | Stack Height (ft): | |
| | Stack Diameter (ft): | |
| | Exit Gas Velocity (ft/s): | |
| | Exit Gas Temp (F): | |
| | Exit Gas Flow Rate (acfm): | |
| Company Release Point ID: | Release Point Latitude: | 43.737071 |
| FUGITIVES | Release Point Longitude: | -105.837423 |
| | Release Height (ft): 4 | |
| Company Release Point Description: | | |
| Potential leaks | | |
| | | |
| | | |
| Company Release Point ID: | Release Point Latitude: | |
| | Release Point Longitude: | |
| | Release Height (ft): | |
| Company Release Point Description: | | _ |
| company necesser one bescription. | _ | |
| | | |
| | | |
| Company Release Point ID: | Delegas Delich Letter | |
| Company Release Form ID. | Release Point Latitude: | |
| | Release Point Longitude: | |
| | Release Height (ft): | |
| Company Release Point Description: | | |
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